

## PROPERTY TABLES AND CHARTS (SI UNITS)

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TABLE A-1

Molar mass, gas constant, and ideal-gas specific heats of some substances

Substance	Molar Mass <i>M</i> , kg/kmol	Gas Constant <i>R</i> , kJ/kg·K*	Specific Heat Data at 25°C		
			<i>c<sub>p</sub></i> , kJ/kg·K	<i>c<sub>v</sub></i> , kJ/kg·K	<i>k</i> = <i>c<sub>p</sub></i> / <i>c<sub>v</sub></i>
Air	28.97	0.2870	1.005	0.7180	1.400
Ammonia, NH <sub>3</sub>	17.03	0.4882	2.093	1.605	1.304
Argon, Ar	39.95	0.2081	0.5203	0.3122	1.667
Bromine, Br <sub>2</sub>	159.81	0.05202	0.2253	0.1732	1.300
Isobutane, C <sub>4</sub> H <sub>10</sub>	58.12	0.1430	1.663	1.520	1.094
<i>n</i> -Butane, C <sub>4</sub> H <sub>10</sub>	58.12	0.1430	1.694	1.551	1.092
Carbon dioxide, CO <sub>2</sub>	44.01	0.1889	0.8439	0.6550	1.288
Carbon monoxide, CO	28.01	0.2968	1.039	0.7417	1.400
Chlorine, Cl <sub>2</sub>	70.905	0.1173	0.4781	0.3608	1.325
Chlorodifluoromethane (R-22), CHClF <sub>2</sub>	86.47	0.09615	0.6496	0.5535	1.174
Ethane, C <sub>2</sub> H <sub>6</sub>	30.070	0.2765	1.744	1.468	1.188
Ethylene, C <sub>2</sub> H <sub>4</sub>	28.054	0.2964	1.527	1.231	1.241
Fluorine, F <sub>2</sub>	38.00	0.2187	0.8237	0.6050	1.362
Helium, He	4.003	2.077	5.193	3.116	1.667
<i>n</i> -Heptane, C <sub>7</sub> H <sub>16</sub>	100.20	0.08297	1.649	1.566	1.053
<i>n</i> -Hexane, C <sub>6</sub> H <sub>14</sub>	86.18	0.09647	1.654	1.558	1.062
Hydrogen, H <sub>2</sub>	2.016	4.124	14.30	10.18	1.405
Krypton, Kr	83.80	0.09921	0.2480	0.1488	1.667
Methane, CH <sub>4</sub>	16.04	0.5182	2.226	1.708	1.303
Neon, Ne	20.183	0.4119	1.030	0.6180	1.667
Nitrogen, N <sub>2</sub>	28.01	0.2968	1.040	0.7429	1.400
Nitric oxide, NO	30.006	0.2771	0.9992	0.7221	1.384
Nitrogen dioxide, NO <sub>2</sub>	46.006	0.1889	0.8060	0.6171	1.306
Oxygen, O <sub>2</sub>	32.00	0.2598	0.9180	0.6582	1.395
<i>n</i> -Pentane, C <sub>5</sub> H <sub>12</sub>	72.15	0.1152	1.664	1.549	1.074
Propane, C <sub>3</sub> H <sub>8</sub>	44.097	0.1885	1.669	1.480	1.127
Propylene, C <sub>3</sub> H <sub>6</sub>	42.08	0.1976	1.531	1.333	1.148
Steam, H <sub>2</sub> O	18.015	0.4615	1.865	1.403	1.329
Sulfur dioxide, SO <sub>2</sub>	64.06	0.1298	0.6228	0.4930	1.263
Tetrachloromethane, CCl <sub>4</sub>	153.82	0.05405	0.5415	0.4875	1.111
Tetrafluoroethane (R-134a), C <sub>2</sub> H <sub>2</sub> F <sub>4</sub>	102.03	0.08149	0.8334	0.7519	1.108
Trifluoroethane (R-143a), C <sub>2</sub> H <sub>3</sub> F <sub>3</sub>	84.04	0.09893	0.9291	0.8302	1.119
Xenon, Xe	131.30	0.06332	0.1583	0.09499	1.667

\*The unit kJ/kg·K is equivalent to kPa·m<sup>3</sup>/kg·K. The gas constant is calculated from  $R = R_U/M$ , where  $R_U = 8.31447$  kJ/kmol·K is the universal gas constant and  $M$  is the molar mass.

Source: Specific heat values are obtained primarily from the property routines prepared by The National Institute of Standards and Technology (NIST), Gaithersburg, MD.

TABLE A-2

Boiling and freezing point properties

Substance	Boiling Data at 1 atm		Freezing Data		Liquid Properties		
	Normal Boiling Point, °C	Latent Heat of Vaporization $h_{fg}$ , kJ/kg	Freezing Point, °C	Latent Heat of Fusion $h_{if}$ , kJ/kg	Temperature, °C	Density $\rho$ , kg/m <sup>3</sup>	Specific Heat $c_p$ , kJ/kg·K
Ammonia	-33.3	1357	-77.7	322.4	-33.3	682	4.43
					-20	665	4.52
					0	639	4.60
					25	602	4.80
					-185.6	1394	1.14
Argon	-185.9	161.6	-189.3	28	-185.6	1394	1.14
Benzene	80.2	394	5.5	126	20	879	1.72
Brine (20% sodium chloride by mass)	103.9	—	-17.4	—	20	1150	3.11
<i>n</i> -Butane	-0.5	385.2	-138.5	80.3	-0.5	601	2.31
Carbon dioxide	-78.4*	230.5 (at 0°C)	-56.6	—	0	298	0.59
Ethanol	78.2	838.3	-114.2	109	25	783	2.46
Ethyl alcohol	78.6	855	-156	108	20	789	2.84
Ethylene glycol	198.1	800.1	-10.8	181.1	20	1109	2.84
Glycerine	179.9	974	18.9	200.6	20	1261	2.32
Helium	-268.9	22.8	—	—	-268.9	146.2	22.8
Hydrogen	-252.8	445.7	-259.2	59.5	-252.8	70.7	10.0
Isobutane	-11.7	367.1	-160	105.7	-11.7	593.8	2.28
Kerosene	204–293	251	-24.9	—	20	820	2.00
Mercury	356.7	294.7	-38.9	11.4	25	13,560	0.139
Methane	-161.5	510.4	-182.2	58.4	-161.5	423	3.49
					-100	301	5.79
					25	787	2.55
Methanol	64.5	1100	-97.7	99.2	25	787	2.55
Nitrogen	-195.8	198.6	-210	25.3	-195.8	809	2.06
					-160	596	2.97
					20	703	2.10
Octane	124.8	306.3	-57.5	180.7	25	910	1.80
Oil (light)	—	—	—	—	20	640	2.0
Oxygen	-183	212.7	-218.8	13.7	-183	1141	1.71
Petroleum	—	230–384	—	—	20	640	2.0
					-42.1	427.8	-187.7
Propane	-42.1	427.8	-187.7	80.0	0	529	2.53
					50	449	3.13
					-50	1443	1.23
					-26.1	1374	1.27
					0	1295	1.34
Refrigerant-134a	-26.1	216.8	-96.6	—	25	1207	1.43
					0	1000	4.22
					25	997	4.18
					50	988	4.18
					75	975	4.19
Water	100	2257	0.0	333.7	100	958	4.22

\* Sublimation temperature. (At pressures below the triple-point pressure of 518 kPa, carbon dioxide exists as a solid or gas. Also, the freezing-point temperature of carbon dioxide is the triple-point temperature of -56.5°C.)

TABLE A-3

Properties of solid metals

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Aluminum:											
Pure	933	2702	903	237	97.1	302	237	240	231	218	
						482	798	949	1033	1146	
Alloy 2024-T6 (4.5% Cu, 1.5% Mg, 0.6% Mn)	775	2770	875	177	73.0	65	163	186	186		
Alloy 195, Cast (4.5% Cu)						473	787	925	1042		
Beryllium	1550	1850	1825	200	59.2	990	301	161	126	106	90.8
						203	1114	2191	2604	2823	3018
Bismuth	545	9780	122	7.86	6.59	16.5	9.69	7.04			
						112	120	127			
Boron	2573	2500	1107	27.0	9.76	190	55.5	16.8	10.6	9.60	9.85
						128	600	1463	1892	2160	2338
Cadmium	594	8650	231	96.8	48.4	203	99.3	94.7			
						198	222	242			
Chromium	2118	7160	449	93.7	29.1	159	111	90.9	80.7	71.3	65.4
						192	384	484	542	581	616
Cobalt	1769	8862	421	99.2	26.6	167	122	85.4	67.4	58.2	52.1
						236	379	450	503	550	628
Copper:											
Pure	1358	8933	385	401	117	482	413	393	379	366	352
						252	356	397	417	433	451
Commercial bronze (90% Cu, 10% Al)	1293	8800	420	52	14		42	52	59		
							785	160	545		
Phosphor gear bronze (89% Cu, 11% Sn)	1104	8780	355	54	17		41	65	74		
							—	—	—		
Cartridge brass (70% Cu, 30% Zn)	1188	8530	380	110	33.9	75	95	137	149		
							360	395	425		
Constantan (55% Cu, 45% Ni)	1493	8920	384	23	6.71	17	19				
						237	362				
Germanium	1211	5360	322	59.9	34.7	232	96.8	43.2	27.3	19.8	17.4
						190	290	337	348	357	375
Gold	1336	19,300	129	317	127	327	323	311	298	284	270
						109	124	131	135	140	145
Iridium	2720	22,500	130	147	50.3	172	153	144	138	132	126
						90	122	133	138	144	153
Iron:											
Pure	1810	7870	447	80.2	23.1	134	94.0	69.5	54.7	43.3	32.8
						216	384	490	574	680	975
Armco (99.75% pure)		7870	447	72.7	20.7	95.6	80.6	65.7	53.1	42.2	32.3
						215	384	490	574	680	975
Carbon steels:											
Plain carbon (Mn $\leq$ 1% Si $\leq$ 0.1%)		7854	434	60.5	17.7			56.7	48.0	39.2	30.0
								487	559	685	1169
AISI 1010		7832	434	63.9	18.8			58.7	48.8	39.2	31.3
							487	559	685	1168	
Carbon-silicon (Mn $\leq$ 1% 0.1% < Si $\leq$ 0.6%)		7817	446	51.9	14.9			49.8	44.0	37.4	29.3
								501	582	699	971

TABLE A-3

Properties of solid metals (Continued)

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Carbon-manganese-silicon (1% < Mn < 1.65% 0.1% < Si < 0.6%)		8131	434	41.0	11.6			42.2 487	39.7 559	35.0 685	27.6 1090
Chromium (low) steels: $\frac{1}{2}$ Cr- $\frac{1}{4}$ Mo-Si (0.18% C, 0.65% Cr, 0.23% Mo, 0.6% Si)		7822	444	37.7	10.9			38.2	36.7	33.3	26.9
1 Cr- $\frac{1}{2}$ Mo (0.16% C, 1% Cr, 0.54% Mo, 0.39% Si)		7858	442	42.3	12.2			492 42.0	575 39.1	688 34.5	969 27.4
1 Cr-V (0.2% C, 1.02% Cr, 0.15% V)		7836	443	48.9	14.1			492 46.8	575 42.1	688 36.3	969 28.2
Stainless steels: AISI 302		8055	480	15.1	3.91			17.3 512	20.0 559	22.8 585	25.4 606
AISI 304	1670	7900	477	14.9	3.95	9.2 272	12.6 402	16.6 515	19.8 557	22.6 582	25.4 611
AISI 316		8238	468	13.4	3.48			15.2 504	18.3 550	21.3 576	24.2 602
AISI 347		7978	480	14.2	3.71			15.8 513	18.9 559	21.9 585	24.7 606
Lead	601	11,340	129	35.3	24.1	39.7 118	36.7 125	34.0 132	31.4 142		
Magnesium	923	1740	1024	156	87.6	169 649	159 934	153 1074	149 1170	146 1267	
Molybdenum	2894	10,240	251	138	53.7	179 141	143 224	134 261	126 275	118 285	112 295
Nickel: Pure	1728	8900	444	90.7	23.0 232	164 383	107 485	80.2 592	65.6 530	67.6 562	71.8
Nichrome (80% Ni, 20% Cr)	1672	8400	420	12	3.4			14 480	16 525	21 545	
Inconel X-750 (73% Ni, 15% Cr, 6.7% Fe)	1665	8510	439	11.7	3.1	8.7 —	10.3 372	13.5 473	17.0 510	20.5 546	24.0 626
Niobium	2741	8570	265	53.7	23.6	55.2 188	52.6 249	55.2 274	58.2 283	61.3 292	64.4 301
Palladium	1827	12,020	244	71.8	24.5	76.5 168	71.6 227	73.6 251	79.7 261	86.9 271	94.2 281
Platinum: Pure	2045	21,450	133	71.6	25.1	77.5 100	72.6 125	71.8 136	73.2 141	75.6 146	78.7 152
Alloy 60Pt-40Rh (60% Pt, 40% Rh)	1800	16,630	162	47	17.4			52 —	59 —	65 —	69 —
Rhenium	3453	21,100	136	47.9	16.7	58.9 97	51.0 127	46.1 139	44.2 145	44.1 151	44.6 156
Rhodium	2236	12,450	243	150	49.6	186 147	154 220	146 253	136 274	127 293	121 311

**TABLE A-3**

Properties of solid metals (*Concluded*)

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Silicon	1685	2330	712	148	89.2	884	264	98.9	61.9	42.4	31.2
Silver	1235	10,500	235	429	174	259	556	790	867	913	946
						187	225	239	250	262	277
Tantalum	3269	16,600	140	57.5	24.7	59.2	57.5	57.8	58.6	59.4	60.2
Thorium	2023	11,700	118	54.0	39.1	110	133	144	146	149	152
						59.8	54.6	54.5	55.8	56.9	56.9
Tin	505	7310	227	66.6	40.1	99	112	124	134	145	156
						85.2	73.3	62.2			
Titanium	1953	4500	522	21.9	9.32	188	215	243			
						30.5	24.5	20.4	19.4	19.7	20.7
Tungsten	3660	19,300	132	174	68.3	300	465	551	591	633	675
						208	186	159	137	125	118
Uranium	1406	19,070	116	27.6	12.5	87	122	137	142	146	148
						21.7	25.1	29.6	34.0	38.8	43.9
Vanadium	2192	6100	489	30.7	10.3	94	108	125	146	176	180
						35.8	31.3	31.3	33.3	35.7	38.2
Zinc	693	7140	389	116	41.8	258	430	515	540	563	597
						117	118	111	103		
Zirconium	2125	6570	278	22.7	12.4	297	367	402	436		
						33.2	25.2	21.6	20.7	21.6	23.7
						205	264	300	332	342	362

From Frank P. Incropera and David P. DeWitt, *Fundamentals of Heat and Mass Transfer, 3rd ed.*, 1990. This material is used by permission of John Wiley & Sons, Inc.

TABLE A-4

Properties of solid nonmetals

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k$ (W/m-K)/ $c_p$ (J/kg-K)					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg-K	$k$ W/m-K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Aluminum oxide, sapphire	2323	3970	765	46	15.1	450	82	32.4	18.9	13.0	10.5
Aluminum oxide, polycrystalline	2323	3970	765	36.0	11.9	133	55	26.4	15.8	10.4	7.85
Beryllium oxide	2725	3000	1030	272	88.0	—	—	940	1110	1180	1225
								196	111	70	47
								1350	1690	1865	1975
Boron	2573	2500	1105	27.6	9.99	190	52.5	18.7	11.3	8.1	6.3
						—	—	1490	1880	2135	2350
Boron fiber epoxy (30% vol.) composite	590	2080									
$k$ ,    to fibers				2.29		2.10	2.23	2.28			
$k$ , $\perp$ to fibers				0.59		0.37	0.49	0.60			
$c_p$			1122			364	757	1431			
Carbon											
Amorphous	1500	1950	—	1.60	—	0.67	1.18	1.89	21.9	2.37	2.53
						—	—	—	—	—	—
Diamond, type IIa insulator	—	3500	509	2300		10,000	4000	1540			
						21	194	853			
Graphite, pyrolytic	2273	2210									
$k$ ,    to layers				1950		4970	3230	1390	892	667	534
$k$ , $\perp$ to layers				5.70		16.8	9.23	4.09	2.68	2.01	1.60
$c_p$			709			136	411	992	1406	1650	1793
Graphite fiber epoxy (25% vol.) composite	450	1400									
$k$ , heat flow    to fibers				11.1		5.7	8.7	13.0			
$k$ , heat flow $\perp$ to fibers				0.87	0.46	0.68	1.1				
$c_p$			935			337	642	1216			
Pyroceram, Corning 9606	1623	2600	808	3.98	1.89	5.25	4.78	3.64	3.28	3.08	2.96
Silicon carbide	3100	3160	675	490	230	—	—	908	1038	1122	1197
								880	1050	1135	1195
Silicon dioxide, crystalline (quartz)	1883	2650									
$k$ ,    to $c$ -axis				10.4		39	16.4	7.6	5.0	4.2	
$k$ , $\perp$ to $c$ -axis				6.21		20.8	9.5	4.70	3.4	3.1	
$c_p$			745			—	—	885	1075	1250	
Silicon dioxide, polycrystalline (fused silica)	1883	2220	745	1.38	0.834	0.69	1.14	1.51	1.75	2.17	2.87
						—	—	905	1040	1105	1155
Silicon nitride	2173	2400	691	16.0	9.65	—	—	13.9	11.3	9.88	8.76
						—	578	778	937	1063	1155
Sulfur	392	2070	708	0.206	0.141	0.165	0.185				
						403	606				
Thorium dioxide	3573	9110	235	13	6.1			10.2	6.6	4.7	3.68
								255	274	285	295
Titanium dioxide, polycrystalline	2133	4157	710	8.4	2.8			7.01	5.02	8.94	3.46
								805	880	910	930

**TABLE A-5**

Properties of building materials (at a mean temperature of 24°C)

Material	Thickness, $L$ mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ kJ/kg·K	$R$ -value (for listed thickness, $L/k$ ), K·m <sup>2</sup> /W
<b>Building Boards</b>					
Asbestos-cement board	6 mm	1922	—	1.00	0.011
Gypsum of plaster board	10 mm	800	—	1.09	0.057
	13 mm	800	—	—	0.078
Plywood (Douglas fir)	—	545	0.12	1.21	—
	6 mm	545	—	1.21	0.055
	10 mm	545	—	1.21	0.083
	13 mm	545	—	1.21	0.110
	20 mm	545	—	1.21	0.165
Insulated board and sheathing (regular density)	13 mm	288	—	1.30	0.232
	20 mm	288	—	1.30	0.359
Hardboard (high density, standard tempered)	—	1010	0.14	1.34	—
Particle board:					
Medium density	—	800	0.14	1.30	—
Underlayment	16 mm	640	—	1.21	0.144
Wood subfloor	20 mm	—	—	1.38	0.166
<b>Building Membrane</b>					
Vapor-permeable felt	—	—	—	—	0.011
Vapor-seal (2 layers of mopped 0.73 kg/m <sup>2</sup> felt)	—	—	—	—	0.021
<b>Flooring Materials</b>					
Carpet and fibrous pad	—	—	—	1.42	0.367
Carpet and rubber pad	—	—	—	1.38	0.217
Tile (asphalt, linoleum, vinyl)	—	—	—	1.26	0.009
<b>Masonry Materials</b>					
<i>Masonry units:</i>					
Brick, common		1922	0.72	—	—
Brick, face		2082	1.30	—	—
Brick, fire clay		2400	1.34	—	—
		1920	0.90	0.79	—
		1120	0.41	—	—
Concrete blocks (3 oval cores, sand and gravel aggregate)	100 mm	—	0.77	—	0.13
	200 mm	—	1.0	—	0.20
	300 mm	—	1.30	—	0.23
<i>Concretes:</i>					
Lightweight aggregates, (including expanded shale, clay, or slate; expanded slags; cinders; pumice; and scoria)		1920	1.1	—	—
		1600	0.79	0.84	—
		1280	0.54	0.84	—
		960	0.33	—	—
	940	0.18	—	—	—
Cement/lime, mortar, and stucco		1920	1.40	—	—
		1280	0.65	—	—
Stucco		1857	0.72	—	—



TABLE A-5

Properties of building materials (*Concluded*)  
(at a mean temperature of 24°C)

Material	Thickness, <i>L</i> mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, <i>k</i> W/m·K	Specific Heat, $c_p$ kJ/kg·K	<i>R</i> -value (for listed thickness, <i>L/k</i> ), K·m <sup>2</sup> /W
<b>Roofing</b>					
Asbestos-cement shingles		1900	—	1.00	0.037
Asphalt roll roofing		1100	—	1.51	0.026
Asphalt shingles		1100	—	1.26	0.077
Built-in roofing	10 mm	1100	—	1.46	0.058
Slate	13 mm	—	—	1.26	0.009
Wood shingles (plain and plastic/film faced)		—	—	1.30	0.166
<b>Plastering Materials</b>					
Cement plaster, sand aggregate	19 mm	1860	0.72	0.84	0.026
Gypsum plaster:					
Lightweight aggregate	13 mm	720	—	—	0.055
Sand aggregate	13 mm	1680	0.81	0.84	0.016
Perlite aggregate	—	720	0.22	1.34	—
<b>Siding Material (on flat surfaces)</b>					
Asbestos-cement shingles	—	1900	—	—	0.037
Hardboard siding	11 mm	—	—	1.17	0.12
Wood (drop) siding	25 mm	—	—	1.30	0.139
Wood (plywood) siding lapped	10 mm	—	—	1.21	0.111
Aluminum or steel siding (over sheeting):					
Hollow backed	10 mm	—	—	1.22	0.11
Insulating-board backed	10 mm	—	—	1.34	0.32
Architectural glass	—	2530	1.0	0.84	0.018
<b>Woods</b>					
Hardwoods (maple, oak, etc.)	—	721	0.159	1.26	—
Softwoods (fir, pine, etc.)	—	513	0.115	1.38	—
<b>Metals</b>					
Aluminum (1100)	—	2739	222	0.896	—
Steel, mild	—	7833	45.3	0.502	—
Steel, Stainless	—	7913	15.6	0.456	—

Source: Table A-5 and A-6 are adapted from *ASHRAE, Handbook of Fundamentals* (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, 1993), Chap. 22, Table 4. Used with permission.

**TABLE A-6**

Properties of insulating materials  
(at a mean temperature of 24°C)

Material	Thickness, <i>L</i> mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, <i>k</i> W/m·K	Specific Heat, $c_p$ kJ/kg·K	<i>R</i> -value (for listed thickness, <i>L/k</i> ), K·m <sup>2</sup> /W
<b>Blanket and Batt</b>					
Mineral fiber (fibrous form)	50 to 70 mm	4.8–32	—	0.71–0.96	1.23
processed from rock, slag, or glass)	75 to 90 mm	4.8–32	—	0.71–0.96	1.94
	135 to 165 mm	4.8–32	—	0.71–0.96	3.32
<b>Board and Slab</b>					
Cellular glass		136	0.055	1.0	—
Glass fiber (organic bonded)		64–144	0.036	0.96	—
Expanded polystyrene (molded beads)		16	0.040	1.2	—
Expanded polyurethane ( <i>R</i> -11 expanded)		24	0.023	1.6	—
Expanded perlite (organic bonded)		16	0.052	1.26	—
Expanded rubber (rigid)		72	0.032	1.68	—
Mineral fiber with resin binder		240	0.042	0.71	—
Cork		120	0.039	1.80	—
<b>Sprayed or Formed in Place</b>					
Polyurethane foam		24–40	0.023–0.026	—	—
Glass fiber		56–72	0.038–0.039	—	—
Urethane, two-part mixture (rigid foam)		70	0.026	1.045	—
Mineral wool granules with asbestos/ inorganic binders (sprayed)		190	0.046	—	—
<b>Loose Fill</b>					
Mineral fiber (rock, slag, or glass)	~75 to 125 mm	9.6–32	—	0.71	1.94
	~165 to 222 mm	9.6–32	—	0.71	3.35
	~191 to 254 mm	—	—	0.71	3.87
	~185 mm	—	—	0.71	5.28
Silica aerogel		122	0.025	—	—
Vermiculite (expanded)		122	0.068	—	—
Perlite, expanded		32–66	0.039–0.045	1.09	—
Sawdust or shavings		128–240	0.065	1.38	—
Cellulosic insulation (milled paper or wood pulp)		37–51	0.039–0.046	—	—
<b>Roof Insulation</b>					
Cellular glass	—	144	0.058	1.0	—
Preformed, for use above deck	13 mm	—	—	1.0	0.24
	25 mm	—	—	2.1	0.49
	50 mm	—	—	3.9	0.93
<b>Reflective Insulation</b>					
Silica powder (evacuated)		160	0.0017	—	—
Aluminum foil separating fluffy glass mats; 10–12 layers (evacuated); for cryogenic applications (150 K)		40	0.00016	—	—
Aluminum foil and glass paper laminate; 75–150 layers (evacuated); for cryogenic applications (150 K)		120	0.000017	—	—

**TABLE A-7**

Properties of common foods  
(a) Specific heats and freezing-point properties

Food	Water content, <sup>a</sup> % (mass)	Freezing Point <sup>a</sup> °C	Specific heat, <sup>b</sup> kJ/kg·K		Latent Heat of Fusion, <sup>c</sup> kJ/kg	Food	Water content, <sup>a</sup> % (mass)	Freezing Point <sup>a</sup> °C	Specific heat, <sup>b</sup> kJ/kg·K		Latent Heat of Fusion, <sup>c</sup> kJ/kg
			Above Freezing	Below Freezing					Above Freezing	Below Freezing	
<b>Vegetables</b>											
Artichokes	84	-1.2	3.65	1.90	281	Peaches	89	-0.9	3.82	1.96	297
Asparagus	93	-0.6	3.96	2.01	311	Pears	83	-1.6	3.62	1.89	277
Beans, snap	89	-0.7	3.82	1.96	297	Pineapples	85	-1.0	3.69	1.91	284
Broccoli	90	-0.6	3.86	1.97	301	Plums	86	-0.8	3.72	1.92	287
Cabbage	92	-0.9	3.92	2.00	307	Quinces	85	-2.0	3.69	1.91	284
Carrots	88	-1.4	3.79	1.95	294	Raisins	18	—	—	1.07	60
Cauliflower	92	-0.8	3.92	2.00	307	Strawberries	90	-0.8	3.86	1.97	301
Celery	94	-0.5	3.99	2.02	314	Tangerines	87	-1.1	3.75	1.94	291
Corn, sweet	74	-0.6	3.32	1.77	247	Watermelon	93	-0.4	3.96	2.01	311
Cucumbers	96	-0.5	4.06	2.05	321	<b>Fish/Seafood</b>					
Eggplant	93	-0.8	3.96	2.01	311	Cod, whole	78	-2.2	3.45	1.82	261
Horseradish	75	-1.8	3.35	1.78	251	Halibut, whole	75	-2.2	3.35	1.78	251
Leeks	85	-0.7	3.69	1.91	284	Lobster	79	-2.2	3.49	1.84	264
Lettuce	95	-0.2	4.02	2.04	317	Mackerel	57	-2.2	2.75	1.56	190
Mushrooms	91	-0.9	3.89	1.99	304	Salmon, whole	64	-2.2	2.98	1.65	214
Okra	90	-1.8	3.86	1.97	301	Shrimp	83	-2.2	3.62	1.89	277
Onions, green	89	-0.9	3.82	1.96	297	<b>Meats</b>					
Onions, dry	88	-0.8	3.79	1.95	294	Beef carcass	49	-1.7	2.48	1.46	164
Parsley	85	-1.1	3.69	1.91	284	Liver	70	-1.7	3.18	1.72	234
Peas, green	74	-0.6	3.32	1.77	247	Round, beef	67	—	3.08	1.68	224
Peppers, sweet	92	-0.7	3.92	2.00	307	Sirloin, beef	56	—	2.72	1.55	187
Potatoes	78	-0.6	3.45	1.82	261	Chicken	74	-2.8	3.32	1.77	247
Pumpkins	91	-0.8	3.89	1.99	304	Lamb leg	65	—	3.02	1.66	217
Spinach	93	-0.3	3.96	2.01	311	Port carcass	37	—	2.08	1.31	124
Tomatoes, ripe	94	-0.5	3.99	2.02	314	Ham	56	-1.7	2.72	1.55	187
Turnips	92	-1.1	3.92	2.00	307	Pork sausage	38	—	2.11	1.32	127
						Turkey	64	—	2.98	1.65	214
<b>Fruits</b>						<b>Other</b>					
Apples	84	-1.1	3.65	1.90	281	Almonds	5	—	—	0.89	17
Apricots	85	-1.1	3.69	1.91	284	Butter	16	—	—	1.04	53
Avocados	65	-0.3	3.02	1.66	217	Cheese, Cheddar	37	-12.9	2.08	1.31	124
Bananas	75	-0.8	3.35	1.78	251	Cheese, Swiss	39	-10.0	2.15	1.33	130
Blueberries	82	-1.6	3.59	1.87	274	Chocolate milk	1	—	—	0.85	3
Cantaloupes	92	-1.2	3.92	2.00	307	Eggs, whole	74	-0.6	3.32	1.77	247
Cherries, sour	84	-1.7	3.65	1.90	281	Honey	17	—	—	1.05	57
Cherries, sweet	80	-1.8	3.52	1.85	267	Ice cream	63	-5.6	2.95	1.63	210
Figs, dried	23	—	—	1.13	77	Milk, whole	88	-0.6	3.79	1.95	294
Figs, fresh	78	-2.4	3.45	1.82	261	Peanuts	6	—	—	0.92	20
Grapefruit	89	-1.1	3.82	1.96	297	Peanuts, roasted	2	—	—	0.87	7
Grapes	82	-1.1	3.59	1.87	274	Pecans	3	—	—	0.87	10
Lemons	89	-1.4	3.82	1.96	297	Walnuts	4	—	—	0.88	13
Olives	75	-1.4	3.35	1.78	251						
Oranges	87	-0.8	3.75	1.94	291						

Sources: <sup>a</sup>Water content and freezing-point data are from ASHRAE, *Handbook of Fundamentals*, SI version (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), Chap. 30. Table 1. Used with permission. Freezing point is the temperature at which freezing starts for fruits and vegetables, and the average freezing temperature for other foods.

<sup>b</sup>Specific heat data are based on the specific heat values of a water and ice at 0°C and are determined from Siebel's formulas:  $c_{p, fresh} = 3.35 \times (\text{Water content}) + 0.84$ , above freezing, and  $c_{p, frozen} = 1.26 \times (\text{Water content}) + 0.84$ , below freezing.

<sup>c</sup>The latent heat of fusion is determined by multiplying the heat of fusion of water (334 kJ/kg) by the water content of the food.

TABLE A-7

Properties of common foods (Concluded)

(b) Other properties

Food	Water Content, % (mass)	Temperature, $T$ °C	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Thermal Diffusivity, $\alpha$ m <sup>2</sup> /s	Specific Heat, $c_p$ kJ/kg·K
<b>Fruits/Vegetables</b>						
Apple juice	87	20	1000	0.559	$0.14 \times 10^{-6}$	3.86
Apples	85	8	840	0.418	$0.13 \times 10^{-6}$	3.81
Apples, dried	41.6	23	856	0.219	$0.096 \times 10^{-6}$	2.72
Apricots, dried	43.6	23	1320	0.375	$0.11 \times 10^{-6}$	2.77
Bananas, fresh	76	27	980	0.481	$0.14 \times 10^{-6}$	3.59
Broccoli	—	-6	560	0.385	—	—
Cherries, fresh	92	0-30	1050	0.545	$0.13 \times 10^{-6}$	3.99
Figs	40.4	23	1241	0.310	$0.096 \times 10^{-6}$	2.69
Grape juice	89	20	1000	0.567	$0.14 \times 10^{-6}$	3.91
Peaches	89	2-32	960	0.526	$0.14 \times 10^{-6}$	3.91
Plums	—	-16	610	0.247	—	—
Potatoes	78	0-70	1055	0.498	$0.13 \times 10^{-6}$	3.64
Raisins	32	23	1380	0.376	$0.11 \times 10^{-6}$	2.48
<b>Meats</b>						
Beef, ground	67	6	950	0.406	$0.13 \times 10^{-6}$	3.36
Beef, lean	74	3	1090	0.471	$0.13 \times 10^{-6}$	3.54
Beef fat	0	35	810	0.190	—	—
Beef liver	72	35	—	0.448	—	3.49
Cat food	39.7	23	1140	0.326	$0.11 \times 10^{-6}$	2.68
Chicken breast	75	0	1050	0.476	$0.13 \times 10^{-6}$	3.56
Dog food	30.6	23	1240	0.319	$0.11 \times 10^{-6}$	2.45
Fish, cod	81	3	1180	0.534	$0.12 \times 10^{-6}$	3.71
Fish, salmon	67	3	—	0.531	—	3.36
Ham	71.8	20	1030	0.480	$0.14 \times 10^{-6}$	3.48
Lamb	72	20	1030	0.456	$0.13 \times 10^{-6}$	3.49
Pork, lean	72	4	1030	0.456	$0.13 \times 10^{-6}$	3.49
Turkey breast	74	3	1050	0.496	$0.13 \times 10^{-6}$	3.54
Veal	75	20	1060	0.470	$0.13 \times 10^{-6}$	3.56
<b>Other</b>						
Butter	16	4	—	0.197	—	2.08
Chocolate cake	31.9	23	340	0.106	$0.12 \times 10^{-6}$	2.48
Margarine	16	5	1000	0.233	$0.11 \times 10^{-6}$	2.08
Milk, skimmed	91	20	—	0.566	—	3.96
Milk, whole	88	28	—	0.580	—	3.89
Olive oil	0	32	910	0.168	—	—
Peanut oil	0	4	920	0.168	—	—
Water	100	0	1000	0.569	$0.14 \times 10^{-6}$	4.217
	100	30	995	0.618	$0.15 \times 10^{-6}$	4.178
White cake	32.3	23	450	0.082	$0.10 \times 10^{-6}$	2.49

Source: Data obtained primarily from ASHRAE, *Handbook of Fundamentals*, SI version (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), Chap. 30, Tables 7 and 9. Used with permission.

Most specific heats are calculated from  $c_p = 1.68 + 2.51 \times (\text{Water content})$ , which is a good approximation in the temperature range of 3 to 32°C. Most thermal diffusivities are calculated from  $\alpha = k/\rho c_p$ . Property values given here are valid for the specific water content.

TABLE A-8

Properties of miscellaneous materials  
(Values are at 300 K unless indicated otherwise)

Material	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ J/kg·K	Material	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ J/kg·K
Asphalt	2115	0.062	920	Ice			
Bakelite	1300	1.4	1465	273 K	920	1.88	2040
Brick, refractory				253 K	922	2.03	1945
Chrome brick				173 K	928	3.49	1460
473 K	3010	2.3	835	Leather, sole	998	0.159	—
823 K	—	2.5	—	Linoleum	535	0.081	—
1173 K	—	2.0	—		1180	0.186	—
Fire clay, burnt				Mica	2900	0.523	—
1600 K				Paper	930	0.180	1340
773 K	2050	1.0	960	Plastics			
1073 K	—	1.1	—	Plexiglass	1190	0.19	1465
1373 K	—	1.1	—	Teflon			
Fire clay, burnt				300 K	2200	0.35	1050
1725 K				400 K	—	0.45	—
773 K	2325	1.3	960	Lexan	1200	0.19	1260
1073 K	—	1.4	—	Nylon	1145	0.29	—
1373 K	—	1.4	—	Polypropylene	910	0.12	1925
Fire clay brick				Polyester	1395	0.15	1170
478 K	2645	1.0	960	PVC, vinyl	1470	0.1	840
922 K	—	1.5	—	Porcelain	2300	1.5	—
1478 K	—	1.8	—	Rubber, natural	1150	0.28	—
Magnesite				Rubber, vulcanized			
478 K	—	3.8	1130	Soft	1100	0.13	2010
922 K	—	2.8	—	Hard	1190	0.16	—
1478 K	—	1.9	—	Sand	1515	0.2–1.0	800
Chicken meat, white (74.4% water content)				Snow, fresh	100	0.60	—
198 K	—	1.60	—	Snow, 273 K	500	2.2	—
233 K	—	1.49	—	Soil, dry	1500	1.0	1900
253 K	—	1.35	—	Soil, wet	1900	2.0	2200
273 K	—	0.48	—	Sugar	1600	0.58	—
293 K	—	0.49	—	Tissue, human			
Clay, dry	1550	0.930	—	Skin	—	0.37	—
Clay, wet	1495	1.675	—	Fat layer	—	0.2	—
Coal, anthracite	1350	0.26	1260	Muscle	—	0.41	—
Concrete (stone mix)	2300	1.4	880	Vaseline	—	0.17	—
Cork	86	0.048	2030	Wood, cross-grain			
Cotton	80	0.06	1300	Balsa	140	0.055	—
Fat	—	0.17	—	Fir	415	0.11	2720
Glass				Oak	545	0.17	2385
Window	2800	0.7	750	White pine	435	0.11	—
Pyrex	2225	1–1.4	835	Yellow pine	640	0.15	2805
Crown	2500	1.05	—	Wood, radial			
Lead	3400	0.85	—	Oak	545	0.19	2385
				Fir	420	0.14	2720
				Wool, ship	145	0.05	—

Source: Compiled from various sources.

TABLE A-9

Properties of saturated water

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> <sub>sat</sub> , kPa	Density <i>ρ</i> , kg/m <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , kJ/kg	Specific Heat <i>c</i> <sub>p</sub> , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity <i>μ</i> , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient <i>β</i> , 1/K
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
0.01	0.6113	999.8	0.0048	2501	4217	1854	0.561	0.0171	1.792 × 10 <sup>-3</sup>	0.922 × 10 <sup>-5</sup>	13.5	1.00	-0.068 × 10 <sup>-3</sup>
5	0.8721	999.9	0.0068	2490	4205	1857	0.571	0.0173	1.519 × 10 <sup>-3</sup>	0.934 × 10 <sup>-5</sup>	11.2	1.00	0.015 × 10 <sup>-3</sup>
10	1.2276	999.7	0.0094	2478	4194	1862	0.580	0.0176	1.307 × 10 <sup>-3</sup>	0.946 × 10 <sup>-5</sup>	9.45	1.00	0.733 × 10 <sup>-3</sup>
15	1.7051	999.1	0.0128	2466	4185	1863	0.589	0.0179	1.138 × 10 <sup>-3</sup>	0.959 × 10 <sup>-5</sup>	8.09	1.00	0.138 × 10 <sup>-3</sup>
20	2.339	998.0	0.0173	2454	4182	1867	0.598	0.0182	1.002 × 10 <sup>-3</sup>	0.973 × 10 <sup>-5</sup>	7.01	1.00	0.195 × 10 <sup>-3</sup>
25	3.169	997.0	0.0231	2442	4180	1870	0.607	0.0186	0.891 × 10 <sup>-3</sup>	0.987 × 10 <sup>-5</sup>	6.14	1.00	0.247 × 10 <sup>-3</sup>
30	4.246	996.0	0.0304	2431	4178	1875	0.615	0.0189	0.798 × 10 <sup>-3</sup>	1.001 × 10 <sup>-5</sup>	5.42	1.00	0.294 × 10 <sup>-3</sup>
35	5.628	994.0	0.0397	2419	4178	1880	0.623	0.0192	0.720 × 10 <sup>-3</sup>	1.016 × 10 <sup>-5</sup>	4.83	1.00	0.337 × 10 <sup>-3</sup>
40	7.384	992.1	0.0512	2407	4179	1885	0.631	0.0196	0.653 × 10 <sup>-3</sup>	1.031 × 10 <sup>-5</sup>	4.32	1.00	0.377 × 10 <sup>-3</sup>
45	9.593	990.1	0.0655	2395	4180	1892	0.637	0.0200	0.596 × 10 <sup>-3</sup>	1.046 × 10 <sup>-5</sup>	3.91	1.00	0.415 × 10 <sup>-3</sup>
50	12.35	988.1	0.0831	2383	4181	1900	0.644	0.0204	0.547 × 10 <sup>-3</sup>	1.062 × 10 <sup>-5</sup>	3.55	1.00	0.451 × 10 <sup>-3</sup>
55	15.76	985.2	0.1045	2371	4183	1908	0.649	0.0208	0.504 × 10 <sup>-3</sup>	1.077 × 10 <sup>-5</sup>	3.25	1.00	0.484 × 10 <sup>-3</sup>
60	19.94	983.3	0.1304	2359	4185	1916	0.654	0.0212	0.467 × 10 <sup>-3</sup>	1.093 × 10 <sup>-5</sup>	2.99	1.00	0.517 × 10 <sup>-3</sup>
65	25.03	980.4	0.1614	2346	4187	1926	0.659	0.0216	0.433 × 10 <sup>-3</sup>	1.110 × 10 <sup>-5</sup>	2.75	1.00	0.548 × 10 <sup>-3</sup>
70	31.19	977.5	0.1983	2334	4190	1936	0.663	0.0221	0.404 × 10 <sup>-3</sup>	1.126 × 10 <sup>-5</sup>	2.55	1.00	0.578 × 10 <sup>-3</sup>
75	38.58	974.7	0.2421	2321	4193	1948	0.667	0.0225	0.378 × 10 <sup>-3</sup>	1.142 × 10 <sup>-5</sup>	2.38	1.00	0.607 × 10 <sup>-3</sup>
80	47.39	971.8	0.2935	2309	4197	1962	0.670	0.0230	0.355 × 10 <sup>-3</sup>	1.159 × 10 <sup>-5</sup>	2.22	1.00	0.653 × 10 <sup>-3</sup>
85	57.83	968.1	0.3536	2296	4201	1977	0.673	0.0235	0.333 × 10 <sup>-3</sup>	1.176 × 10 <sup>-5</sup>	2.08	1.00	0.670 × 10 <sup>-3</sup>
90	70.14	965.3	0.4235	2283	4206	1993	0.675	0.0240	0.315 × 10 <sup>-3</sup>	1.193 × 10 <sup>-5</sup>	1.96	1.00	0.702 × 10 <sup>-3</sup>
95	84.55	961.5	0.5045	2270	4212	2010	0.677	0.0246	0.297 × 10 <sup>-3</sup>	1.210 × 10 <sup>-5</sup>	1.85	1.00	0.716 × 10 <sup>-3</sup>
100	101.33	957.9	0.5978	2257	4217	2029	0.679	0.0251	0.282 × 10 <sup>-3</sup>	1.227 × 10 <sup>-5</sup>	1.75	1.00	0.750 × 10 <sup>-3</sup>
110	143.27	950.6	0.8263	2230	4229	2071	0.682	0.0262	0.255 × 10 <sup>-3</sup>	1.261 × 10 <sup>-5</sup>	1.58	1.00	0.798 × 10 <sup>-3</sup>
120	198.53	943.4	1.121	2203	4244	2120	0.683	0.0275	0.232 × 10 <sup>-3</sup>	1.296 × 10 <sup>-5</sup>	1.44	1.00	0.858 × 10 <sup>-3</sup>
130	270.1	934.6	1.496	2174	4263	2177	0.684	0.0288	0.213 × 10 <sup>-3</sup>	1.330 × 10 <sup>-5</sup>	1.33	1.01	0.913 × 10 <sup>-3</sup>
140	361.3	921.7	1.965	2145	4286	2244	0.683	0.0301	0.197 × 10 <sup>-3</sup>	1.365 × 10 <sup>-5</sup>	1.24	1.02	0.970 × 10 <sup>-3</sup>
150	475.8	916.6	2.546	2114	4311	2314	0.682	0.0316	0.183 × 10 <sup>-3</sup>	1.399 × 10 <sup>-5</sup>	1.16	1.02	1.025 × 10 <sup>-3</sup>
160	617.8	907.4	3.256	2083	4340	2420	0.680	0.0331	0.170 × 10 <sup>-3</sup>	1.434 × 10 <sup>-5</sup>	1.09	1.05	1.145 × 10 <sup>-3</sup>
170	791.7	897.7	4.119	2050	4370	2490	0.677	0.0347	0.160 × 10 <sup>-3</sup>	1.468 × 10 <sup>-5</sup>	1.03	1.05	1.178 × 10 <sup>-3</sup>
180	1,002.1	887.3	5.153	2015	4410	2590	0.673	0.0364	0.150 × 10 <sup>-3</sup>	1.502 × 10 <sup>-5</sup>	0.983	1.07	1.210 × 10 <sup>-3</sup>
190	1,254.4	876.4	6.388	1979	4460	2710	0.669	0.0382	0.142 × 10 <sup>-3</sup>	1.537 × 10 <sup>-5</sup>	0.947	1.09	1.280 × 10 <sup>-3</sup>
200	1,553.8	864.3	7.852	1941	4500	2840	0.663	0.0401	0.134 × 10 <sup>-3</sup>	1.571 × 10 <sup>-5</sup>	0.910	1.11	1.350 × 10 <sup>-3</sup>
220	2,318	840.3	11.60	1859	4610	3110	0.650	0.0442	0.122 × 10 <sup>-3</sup>	1.641 × 10 <sup>-5</sup>	0.865	1.15	1.520 × 10 <sup>-3</sup>
240	3,344	813.7	16.73	1767	4760	3520	0.632	0.0487	0.111 × 10 <sup>-3</sup>	1.712 × 10 <sup>-5</sup>	0.836	1.24	1.720 × 10 <sup>-3</sup>
260	4,688	783.7	23.69	1663	4970	4070	0.609	0.0540	0.102 × 10 <sup>-3</sup>	1.788 × 10 <sup>-5</sup>	0.832	1.35	2.000 × 10 <sup>-3</sup>
280	6,412	750.8	33.15	1544	5280	4835	0.581	0.0605	0.094 × 10 <sup>-3</sup>	1.870 × 10 <sup>-5</sup>	0.854	1.49	2.380 × 10 <sup>-3</sup>
300	8,581	713.8	46.15	1405	5750	5980	0.548	0.0695	0.086 × 10 <sup>-3</sup>	1.965 × 10 <sup>-5</sup>	0.902	1.69	2.950 × 10 <sup>-3</sup>
320	11,274	667.1	64.57	1239	6540	7900	0.509	0.0836	0.078 × 10 <sup>-3</sup>	2.084 × 10 <sup>-5</sup>	1.00	1.97	
340	14,586	610.5	92.62	1028	8240	11,870	0.469	0.110	0.070 × 10 <sup>-3</sup>	2.255 × 10 <sup>-5</sup>	1.23	2.43	
360	18,651	528.3	144.0	720	14,690	25,800	0.427	0.178	0.060 × 10 <sup>-3</sup>	2.571 × 10 <sup>-5</sup>	2.06	3.73	
374.14	22,090	317.0	317.0	0	—	—	—	—	0.043 × 10 <sup>-3</sup>	4.313 × 10 <sup>-5</sup>			

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/Pr$ . The temperatures 0.01°C, 100°C, and 374.14°C are the triple-, boiling-, and critical-point temperatures of water, respectively. The properties listed above (except the vapor density) can be used at any pressure with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Viscosity and thermal conductivity data are from J. V. Sengers and J. T. R. Watson, *Journal of Physical and Chemical Reference Data* 15 (1986), pp. 1291–1322. Other data are obtained from various sources or calculated.

TABLE A-10

Properties of saturated refrigerant-134a

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> , kPa	Density $\rho$ , kg/m <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , kJ/kg	Specific Heat <i>c</i> <sub>p</sub> , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity $\mu$ , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/K	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	51.2	1418	2.773	225.9	1254	748.6	0.1101	0.00811	4.878 × 10 <sup>-4</sup>	2.550 × 10 <sup>-6</sup>	5.558	0.235	0.00205	0.01760
-35	66.2	1403	3.524	222.7	1264	764.1	0.1084	0.00862	4.509 × 10 <sup>-4</sup>	3.003 × 10 <sup>-6</sup>	5.257	0.266	0.00209	0.01682
-30	84.4	1389	4.429	219.5	1273	780.2	0.1066	0.00913	4.178 × 10 <sup>-4</sup>	3.504 × 10 <sup>-6</sup>	4.992	0.299	0.00215	0.01604
-25	106.5	1374	5.509	216.3	1283	797.2	0.1047	0.00963	3.882 × 10 <sup>-4</sup>	4.054 × 10 <sup>-6</sup>	4.757	0.335	0.00220	0.01527
-20	132.8	1359	6.787	213.0	1294	814.9	0.1028	0.01013	3.614 × 10 <sup>-4</sup>	4.651 × 10 <sup>-6</sup>	4.548	0.374	0.00227	0.01451
-15	164.0	1343	8.288	209.5	1306	833.5	0.1009	0.01063	3.371 × 10 <sup>-4</sup>	5.295 × 10 <sup>-6</sup>	4.363	0.415	0.00233	0.01376
-10	200.7	1327	10.04	206.0	1318	853.1	0.0989	0.01112	3.150 × 10 <sup>-4</sup>	5.982 × 10 <sup>-6</sup>	4.198	0.459	0.00241	0.01302
-5	243.5	1311	12.07	202.4	1330	873.8	0.0968	0.01161	2.947 × 10 <sup>-4</sup>	6.709 × 10 <sup>-6</sup>	4.051	0.505	0.00249	0.01229
0	293.0	1295	14.42	198.7	1344	895.6	0.0947	0.01210	2.761 × 10 <sup>-4</sup>	7.471 × 10 <sup>-6</sup>	3.919	0.553	0.00258	0.01156
5	349.9	1278	17.12	194.8	1358	918.7	0.0925	0.01259	2.589 × 10 <sup>-4</sup>	8.264 × 10 <sup>-6</sup>	3.802	0.603	0.00269	0.01084
10	414.9	1261	20.22	190.8	1374	943.2	0.0903	0.01308	2.430 × 10 <sup>-4</sup>	9.081 × 10 <sup>-6</sup>	3.697	0.655	0.00280	0.01014
15	488.7	1244	23.75	186.6	1390	969.4	0.0880	0.01357	2.281 × 10 <sup>-4</sup>	9.915 × 10 <sup>-6</sup>	3.604	0.708	0.00293	0.00944
20	572.1	1226	27.77	182.3	1408	997.6	0.0856	0.01406	2.142 × 10 <sup>-4</sup>	1.075 × 10 <sup>-5</sup>	3.521	0.763	0.00307	0.00876
25	665.8	1207	32.34	177.8	1427	1028	0.0833	0.01456	2.012 × 10 <sup>-4</sup>	1.160 × 10 <sup>-5</sup>	3.448	0.819	0.00324	0.00808
30	770.6	1188	37.53	173.1	1448	1061	0.0808	0.01507	1.888 × 10 <sup>-4</sup>	1.244 × 10 <sup>-5</sup>	3.383	0.877	0.00342	0.00742
35	887.5	1168	43.41	168.2	1471	1098	0.0783	0.01558	1.772 × 10 <sup>-4</sup>	1.327 × 10 <sup>-5</sup>	3.328	0.935	0.00364	0.00677
40	1017.1	1147	50.08	163.0	1498	1138	0.0757	0.01610	1.660 × 10 <sup>-4</sup>	1.408 × 10 <sup>-5</sup>	3.285	0.995	0.00390	0.00613
45	1160.5	1125	57.66	157.6	1529	1184	0.0731	0.01664	1.554 × 10 <sup>-4</sup>	1.486 × 10 <sup>-5</sup>	3.253	1.058	0.00420	0.00550
50	1318.6	1102	66.27	151.8	1566	1237	0.0704	0.01720	1.453 × 10 <sup>-4</sup>	1.562 × 10 <sup>-5</sup>	3.231	1.123	0.00455	0.00489
55	1492.3	1078	76.11	145.7	1608	1298	0.0676	0.01777	1.355 × 10 <sup>-4</sup>	1.634 × 10 <sup>-5</sup>	3.223	1.193	0.00500	0.00429
60	1682.8	1053	87.38	139.1	1659	1372	0.0647	0.01838	1.260 × 10 <sup>-4</sup>	1.704 × 10 <sup>-5</sup>	3.229	1.272	0.00554	0.00372
65	1891.0	1026	100.4	132.1	1722	1462	0.0618	0.01902	1.167 × 10 <sup>-4</sup>	1.771 × 10 <sup>-5</sup>	3.255	1.362	0.00624	0.00315
70	2118.2	996.2	115.6	124.4	1801	1577	0.0587	0.01972	1.077 × 10 <sup>-4</sup>	1.839 × 10 <sup>-5</sup>	3.307	1.471	0.00716	0.00261
75	2365.8	964	133.6	115.9	1907	1731	0.0555	0.02048	9.891 × 10 <sup>-5</sup>	1.908 × 10 <sup>-5</sup>	3.400	1.612	0.00843	0.00209
80	2635.2	928.2	155.3	106.4	2056	1948	0.0521	0.02133	9.011 × 10 <sup>-5</sup>	1.982 × 10 <sup>-5</sup>	3.558	1.810	0.01031	0.00160
85	2928.2	887.1	182.3	95.4	2287	2281	0.0484	0.02233	8.124 × 10 <sup>-5</sup>	2.071 × 10 <sup>-5</sup>	3.837	2.116	0.01336	0.00114
90	3246.9	837.7	217.8	82.2	2701	2865	0.0444	0.02357	7.203 × 10 <sup>-5</sup>	2.187 × 10 <sup>-5</sup>	4.385	2.658	0.01911	0.00071
95	3594.1	772.5	269.3	64.9	3675	4144	0.0396	0.02544	6.190 × 10 <sup>-5</sup>	2.370 × 10 <sup>-5</sup>	5.746	3.862	0.03343	0.00033
100	3975.1	651.7	376.3	33.9	7959	8785	0.0322	0.02989	4.765 × 10 <sup>-5</sup>	2.833 × 10 <sup>-5</sup>	11.77	8.326	0.10047	0.00004

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/\text{Pr}$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: R. Tillner-Roth and H. D. Baehr, "An International Standard Formulation for the Thermodynamic Properties of 1,1,1,2-Tetrafluoroethane (HFC-134a) for Temperatures from 170 K to 455 K and Pressures up to 70 MPa," *J. Phys. Chem. Ref. Data*, Vol. 23, No. 5, 1994; M.J. Assael, N. K. Dalaouti, A. A. Griva, and J. H. Dymond, "Viscosity and Thermal Conductivity of Halogenated Methane and Ethane Refrigerants," *JIR*, Vol. 22, pp. 525-535, 1999; NIST REFPROP 6 program (M. O. McLinden, S. A. Klein, E. W. Lemmon, and A. P. Peskin, Physical and Chemical Properties Division, National Institute of Standards and Technology, Boulder, CO 80303, 1995).

TABLE A-11

Properties of saturated ammonia

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> , kPa	Density $\rho$ , kg/m <sup>3</sup>		Enthalpy of Vaporization <i>h<sub>fg</sub></i> , kJ/kg	Specific Heat <i>c<sub>p</sub></i> , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity $\mu$ , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/K	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	71.66	690.2	0.6435	1389	4414	2242	—	0.01792	$2.926 \times 10^{-4}$	$7.957 \times 10^{-6}$	—	0.9955	0.00176	0.03565
-30	119.4	677.8	1.037	1360	4465	2322	—	0.01898	$2.630 \times 10^{-4}$	$8.311 \times 10^{-6}$	—	1.017	0.00185	0.03341
-25	151.5	671.5	1.296	1345	4489	2369	0.5968	0.01957	$2.492 \times 10^{-4}$	$8.490 \times 10^{-6}$	1.875	1.028	0.00190	0.03229
-20	190.1	665.1	1.603	1329	4514	2420	0.5853	0.02015	$2.361 \times 10^{-4}$	$8.669 \times 10^{-6}$	1.821	1.041	0.00194	0.03118
-15	236.2	658.6	1.966	1313	4538	2476	0.5737	0.02075	$2.236 \times 10^{-4}$	$8.851 \times 10^{-6}$	1.769	1.056	0.00199	0.03007
-10	290.8	652.1	2.391	1297	4564	2536	0.5621	0.02138	$2.117 \times 10^{-4}$	$9.034 \times 10^{-6}$	1.718	1.072	0.00205	0.02896
-5	354.9	645.4	2.886	1280	4589	2601	0.5505	0.02203	$2.003 \times 10^{-4}$	$9.218 \times 10^{-6}$	1.670	1.089	0.00210	0.02786
0	429.6	638.6	3.458	1262	4617	2672	0.5390	0.02270	$1.896 \times 10^{-4}$	$9.405 \times 10^{-6}$	1.624	1.107	0.00216	0.02676
5	516	631.7	4.116	1244	4645	2749	0.5274	0.02341	$1.794 \times 10^{-4}$	$9.593 \times 10^{-6}$	1.580	1.126	0.00223	0.02566
10	615.3	624.6	4.870	1226	4676	2831	0.5158	0.02415	$1.697 \times 10^{-4}$	$9.784 \times 10^{-6}$	1.539	1.147	0.00230	0.02457
15	728.8	617.5	5.729	1206	4709	2920	0.5042	0.02492	$1.606 \times 10^{-4}$	$9.978 \times 10^{-6}$	1.500	1.169	0.00237	0.02348
20	857.8	610.2	6.705	1186	4745	3016	0.4927	0.02573	$1.519 \times 10^{-4}$	$1.017 \times 10^{-5}$	1.463	1.193	0.00245	0.02240
25	1003	602.8	7.809	1166	4784	3120	0.4811	0.02658	$1.438 \times 10^{-4}$	$1.037 \times 10^{-5}$	1.430	1.218	0.00254	0.02132
30	1167	595.2	9.055	1144	4828	3232	0.4695	0.02748	$1.361 \times 10^{-4}$	$1.057 \times 10^{-5}$	1.399	1.244	0.00264	0.02024
35	1351	587.4	10.46	1122	4877	3354	0.4579	0.02843	$1.288 \times 10^{-4}$	$1.078 \times 10^{-5}$	1.372	1.272	0.00275	0.01917
40	1555	579.4	12.03	1099	4932	3486	0.4464	0.02943	$1.219 \times 10^{-4}$	$1.099 \times 10^{-5}$	1.347	1.303	0.00287	0.01810
45	1782	571.3	13.8	1075	4993	3631	0.4348	0.03049	$1.155 \times 10^{-4}$	$1.121 \times 10^{-5}$	1.327	1.335	0.00301	0.01704
50	2033	562.9	15.78	1051	5063	3790	0.4232	0.03162	$1.094 \times 10^{-4}$	$1.143 \times 10^{-5}$	1.310	1.371	0.00316	0.01598
55	2310	554.2	18.00	1025	5143	3967	0.4116	0.03283	$1.037 \times 10^{-4}$	$1.166 \times 10^{-5}$	1.297	1.409	0.00334	0.01493
60	2614	545.2	20.48	997.4	5234	4163	0.4001	0.03412	$9.846 \times 10^{-5}$	$1.189 \times 10^{-5}$	1.288	1.452	0.00354	0.01389
65	2948	536.0	23.26	968.9	5340	4384	0.3885	0.03550	$9.347 \times 10^{-5}$	$1.213 \times 10^{-5}$	1.285	1.499	0.00377	0.01285
70	3312	526.3	26.39	939.0	5463	4634	0.3769	0.03700	$8.879 \times 10^{-5}$	$1.238 \times 10^{-5}$	1.287	1.551	0.00404	0.01181
75	3709	516.2	29.90	907.5	5608	4923	0.3653	0.03862	$8.440 \times 10^{-5}$	$1.264 \times 10^{-5}$	1.296	1.612	0.00436	0.01079
80	4141	505.7	33.87	874.1	5780	5260	0.3538	0.04038	$8.030 \times 10^{-5}$	$1.292 \times 10^{-5}$	1.312	1.683	0.00474	0.00977
85	4609	494.5	38.36	838.6	5988	5659	0.3422	0.04232	$7.646 \times 10^{-5}$	$1.322 \times 10^{-5}$	1.338	1.768	0.00521	0.00876
90	5116	482.8	43.48	800.6	6242	6142	0.3306	0.04447	$7.284 \times 10^{-5}$	$1.354 \times 10^{-5}$	1.375	1.871	0.00579	0.00776
95	5665	470.2	49.35	759.8	6561	6740	0.3190	0.04687	$6.946 \times 10^{-5}$	$1.389 \times 10^{-5}$	1.429	1.999	0.00652	0.00677
100	6257	456.6	56.15	715.5	6972	7503	0.3075	0.04958	$6.628 \times 10^{-5}$	$1.429 \times 10^{-5}$	1.503	2.163	0.00749	0.00579

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/Pr$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Tillner-Roth, Harms-Watzenberg, and Baehr, "Eine neue Fundamentalgleichung für Ammoniak," DKV-Tagungsbericht 20:167–181, 1993; Liley and Desai, "Thermophysical Properties of Refrigerants," ASHRAE, 1993, ISBN 1-1883413-10-9.



TABLE A-12

Properties of saturated propane

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> , kPa	Density $\rho$ , kg/m <sup>3</sup>		Enthalpy of Vaporization $h_{fg}$ , kJ/kg	Specific Heat $c_p$ , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity $\mu$ , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/K	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-120	0.4053	664.7	0.01408	498.3	2003	1115	0.1802	0.00589	$6.136 \times 10^{-4}$	$4.372 \times 10^{-6}$	6.820	0.827	0.00153	0.02630
-110	1.157	654.5	0.03776	489.3	2021	1148	0.1738	0.00645	$5.054 \times 10^{-4}$	$4.625 \times 10^{-6}$	5.878	0.822	0.00157	0.02486
-100	2.881	644.2	0.08872	480.4	2044	1183	0.1672	0.00705	$4.252 \times 10^{-4}$	$4.881 \times 10^{-6}$	5.195	0.819	0.00161	0.02344
-90	6.406	633.8	0.1870	471.5	2070	1221	0.1606	0.00769	$3.635 \times 10^{-4}$	$5.143 \times 10^{-6}$	4.686	0.817	0.00166	0.02202
-80	12.97	623.2	0.3602	462.4	2100	1263	0.1539	0.00836	$3.149 \times 10^{-4}$	$5.409 \times 10^{-6}$	4.297	0.817	0.00171	0.02062
-70	24.26	612.5	0.6439	453.1	2134	1308	0.1472	0.00908	$2.755 \times 10^{-4}$	$5.680 \times 10^{-6}$	3.994	0.818	0.00177	0.01923
-60	42.46	601.5	1.081	443.5	2173	1358	0.1407	0.00985	$2.430 \times 10^{-4}$	$5.956 \times 10^{-6}$	3.755	0.821	0.00184	0.01785
-50	70.24	590.3	1.724	433.6	2217	1412	0.1343	0.01067	$2.158 \times 10^{-4}$	$6.239 \times 10^{-6}$	3.523	0.825	0.00192	0.01649
-40	110.7	578.8	2.629	423.1	2258	1471	0.1281	0.01155	$1.926 \times 10^{-4}$	$6.529 \times 10^{-6}$	3.395	0.831	0.00201	0.01515
-30	167.3	567.0	3.864	412.1	2310	1535	0.1221	0.01250	$1.726 \times 10^{-4}$	$6.827 \times 10^{-6}$	3.266	0.839	0.00213	0.01382
-20	243.8	554.7	5.503	400.3	2368	1605	0.1163	0.01351	$1.551 \times 10^{-4}$	$7.136 \times 10^{-6}$	3.158	0.848	0.00226	0.01251
-10	344.4	542.0	7.635	387.8	2433	1682	0.1107	0.01459	$1.397 \times 10^{-4}$	$7.457 \times 10^{-6}$	3.069	0.860	0.00242	0.01122
0	473.3	528.7	10.36	374.2	2507	1768	0.1054	0.01576	$1.259 \times 10^{-4}$	$7.794 \times 10^{-6}$	2.996	0.875	0.00262	0.00996
5	549.8	521.8	11.99	367.0	2547	1814	0.1028	0.01637	$1.195 \times 10^{-4}$	$7.970 \times 10^{-6}$	2.964	0.883	0.00273	0.00934
10	635.1	514.7	13.81	359.5	2590	1864	0.1002	0.01701	$1.135 \times 10^{-4}$	$8.151 \times 10^{-6}$	2.935	0.893	0.00286	0.00872
15	729.8	507.5	15.85	351.7	2637	1917	0.0977	0.01767	$1.077 \times 10^{-4}$	$8.339 \times 10^{-6}$	2.909	0.905	0.00301	0.00811
20	834.4	500.0	18.13	343.4	2688	1974	0.0952	0.01836	$1.022 \times 10^{-4}$	$8.534 \times 10^{-6}$	2.886	0.918	0.00318	0.00751
25	949.7	492.2	20.68	334.8	2742	2036	0.0928	0.01908	$9.702 \times 10^{-5}$	$8.738 \times 10^{-6}$	2.866	0.933	0.00337	0.00691
30	1076	484.2	23.53	325.8	2802	2104	0.0904	0.01982	$9.197 \times 10^{-5}$	$8.952 \times 10^{-6}$	2.850	0.950	0.00358	0.00633
35	1215	475.8	26.72	316.2	2869	2179	0.0881	0.02061	$8.710 \times 10^{-5}$	$9.178 \times 10^{-6}$	2.837	0.971	0.00384	0.00575
40	1366	467.1	30.29	306.1	2943	2264	0.0857	0.02142	$8.240 \times 10^{-5}$	$9.417 \times 10^{-6}$	2.828	0.995	0.00413	0.00518
45	1530	458.0	34.29	295.3	3026	2361	0.0834	0.02228	$7.785 \times 10^{-5}$	$9.674 \times 10^{-6}$	2.824	1.025	0.00448	0.00463
50	1708	448.5	38.79	283.9	3122	2473	0.0811	0.02319	$7.343 \times 10^{-5}$	$9.950 \times 10^{-6}$	2.826	1.061	0.00491	0.00408
60	2110	427.5	49.66	258.4	3283	2769	0.0765	0.02517	$6.487 \times 10^{-5}$	$1.058 \times 10^{-5}$	2.784	1.164	0.00609	0.00303
70	2580	403.2	64.02	228.0	3595	3241	0.0717	0.02746	$5.649 \times 10^{-5}$	$1.138 \times 10^{-5}$	2.834	1.343	0.00811	0.00204
80	3127	373.0	84.28	189.7	4501	4173	0.0663	0.03029	$4.790 \times 10^{-5}$	$1.249 \times 10^{-5}$	3.251	1.722	0.01248	0.00114
90	3769	329.1	118.6	133.2	6977	7239	0.0595	0.03441	$3.807 \times 10^{-5}$	$1.448 \times 10^{-5}$	4.465	3.047	0.02847	0.00037

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\mu c_p = \nu/\text{Pr}$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Reiner Tillner-Roth, "Fundamental Equations of State," Shaker, Verlag, Aachen, 1998; B. A. Younglove and J. F. Ely, "Thermophysical Properties of Fluids. II Methane, Ethane, Propane, Isobutane, and Normal Butane," *J. Phys. Chem. Ref. Data*, Vol. 16, No. 4, 1987; G.R. Somayajulu, "A Generalized Equation for Surface Tension from the Triple-Point to the Critical-Point," *International Journal of Thermophysics*, Vol. 9, No. 4, 1988.

TABLE A-13

Properties of liquids

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr	Volume Expansion Coeff. $\beta, 1/\text{K}$
<i>Methane (CH<sub>4</sub>)</i>								
-160	420.2	3492	0.1863	$1.270 \times 10^{-7}$	$1.133 \times 10^{-4}$	$2.699 \times 10^{-7}$	2.126	0.00352
-150	405.0	3580	0.1703	$1.174 \times 10^{-7}$	$9.169 \times 10^{-5}$	$2.264 \times 10^{-7}$	1.927	0.00391
-140	388.8	3700	0.1550	$1.077 \times 10^{-7}$	$7.551 \times 10^{-5}$	$1.942 \times 10^{-7}$	1.803	0.00444
-130	371.1	3875	0.1402	$9.749 \times 10^{-8}$	$6.288 \times 10^{-5}$	$1.694 \times 10^{-7}$	1.738	0.00520
-120	351.4	4146	0.1258	$8.634 \times 10^{-8}$	$5.257 \times 10^{-5}$	$1.496 \times 10^{-7}$	1.732	0.00637
-110	328.8	4611	0.1115	$7.356 \times 10^{-8}$	$4.377 \times 10^{-5}$	$1.331 \times 10^{-7}$	1.810	0.00841
-100	301.0	5578	0.0967	$5.761 \times 10^{-8}$	$3.577 \times 10^{-5}$	$1.188 \times 10^{-7}$	2.063	0.01282
-90	261.7	8902	0.0797	$3.423 \times 10^{-8}$	$2.761 \times 10^{-5}$	$1.055 \times 10^{-7}$	3.082	0.02922
<i>Methanol (CH<sub>3</sub>(OH))</i>								
20	788.4	2515	0.1987	$1.002 \times 10^{-7}$	$5.857 \times 10^{-4}$	$7.429 \times 10^{-7}$	7.414	0.00118
30	779.1	2577	0.1980	$9.862 \times 10^{-8}$	$5.088 \times 10^{-4}$	$6.531 \times 10^{-7}$	6.622	0.00120
40	769.6	2644	0.1972	$9.690 \times 10^{-8}$	$4.460 \times 10^{-4}$	$5.795 \times 10^{-7}$	5.980	0.00123
50	760.1	2718	0.1965	$9.509 \times 10^{-8}$	$3.942 \times 10^{-4}$	$5.185 \times 10^{-7}$	5.453	0.00127
60	750.4	2798	0.1957	$9.320 \times 10^{-8}$	$3.510 \times 10^{-4}$	$4.677 \times 10^{-7}$	5.018	0.00132
70	740.4	2885	0.1950	$9.128 \times 10^{-8}$	$3.146 \times 10^{-4}$	$4.250 \times 10^{-7}$	4.655	0.00137
<i>Isobutane (R600a)</i>								
-100	683.8	1881	0.1383	$1.075 \times 10^{-7}$	$9.305 \times 10^{-4}$	$1.360 \times 10^{-6}$	12.65	0.00142
-75	659.3	1970	0.1357	$1.044 \times 10^{-7}$	$5.624 \times 10^{-4}$	$8.531 \times 10^{-7}$	8.167	0.00150
-50	634.3	2069	0.1283	$9.773 \times 10^{-8}$	$3.769 \times 10^{-4}$	$5.942 \times 10^{-7}$	6.079	0.00161
-25	608.2	2180	0.1181	$8.906 \times 10^{-8}$	$2.688 \times 10^{-4}$	$4.420 \times 10^{-7}$	4.963	0.00177
0	580.6	2306	0.1068	$7.974 \times 10^{-8}$	$1.993 \times 10^{-4}$	$3.432 \times 10^{-7}$	4.304	0.00199
25	550.7	2455	0.0956	$7.069 \times 10^{-8}$	$1.510 \times 10^{-4}$	$2.743 \times 10^{-7}$	3.880	0.00232
50	517.3	2640	0.0851	$6.233 \times 10^{-8}$	$1.155 \times 10^{-4}$	$2.233 \times 10^{-7}$	3.582	0.00286
75	478.5	2896	0.0757	$5.460 \times 10^{-8}$	$8.785 \times 10^{-5}$	$1.836 \times 10^{-7}$	3.363	0.00385
100	429.6	3361	0.0669	$4.634 \times 10^{-8}$	$6.483 \times 10^{-5}$	$1.509 \times 10^{-7}$	3.256	0.00628
<i>Glycerin</i>								
0	1276	2262	0.2820	$9.773 \times 10^{-8}$	10.49	$8.219 \times 10^{-3}$	84,101	
5	1273	2288	0.2835	$9.732 \times 10^{-8}$	6.730	$5.287 \times 10^{-3}$	54,327	
10	1270	2320	0.2846	$9.662 \times 10^{-8}$	4.241	$3.339 \times 10^{-3}$	34,561	
15	1267	2354	0.2856	$9.576 \times 10^{-8}$	2.496	$1.970 \times 10^{-3}$	20,570	
20	1264	2386	0.2860	$9.484 \times 10^{-8}$	1.519	$1.201 \times 10^{-3}$	12,671	
25	1261	2416	0.2860	$9.388 \times 10^{-8}$	0.9934	$7.878 \times 10^{-4}$	8,392	
30	1258	2447	0.2860	$9.291 \times 10^{-8}$	0.6582	$5.232 \times 10^{-4}$	5,631	
35	1255	2478	0.2860	$9.195 \times 10^{-8}$	0.4347	$3.464 \times 10^{-4}$	3,767	
40	1252	2513	0.2863	$9.101 \times 10^{-8}$	0.3073	$2.455 \times 10^{-4}$	2,697	
<i>Engine Oil (unused)</i>								
0	899.0	1797	0.1469	$9.097 \times 10^{-8}$	3.814	$4.242 \times 10^{-3}$	46,636	0.00070
20	888.1	1881	0.1450	$8.680 \times 10^{-8}$	0.8374	$9.429 \times 10^{-4}$	10,863	0.00070
40	876.0	1964	0.1444	$8.391 \times 10^{-8}$	0.2177	$2.485 \times 10^{-4}$	2,962	0.00070
60	863.9	2048	0.1404	$7.934 \times 10^{-8}$	0.07399	$8.565 \times 10^{-5}$	1,080	0.00070
80	852.0	2132	0.1380	$7.599 \times 10^{-8}$	0.03232	$3.794 \times 10^{-5}$	499.3	0.00070
100	840.0	2220	0.1367	$7.330 \times 10^{-8}$	0.01718	$2.046 \times 10^{-5}$	279.1	0.00070
120	828.9	2308	0.1347	$7.042 \times 10^{-8}$	0.01029	$1.241 \times 10^{-5}$	176.3	0.00070
140	816.8	2395	0.1330	$6.798 \times 10^{-8}$	0.006558	$8.029 \times 10^{-6}$	118.1	0.00070
150	810.3	2441	0.1327	$6.708 \times 10^{-8}$	0.005344	$6.595 \times 10^{-6}$	98.31	0.00070

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-14

Properties of liquid metals

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr	Volume Expansion Coeff. $\beta, 1/\text{K}$
<i>Mercury (Hg) Melting Point: <math>-39^\circ\text{C}</math></i>								
0	13595	140.4	8.18200	$4.287 \times 10^{-6}$	$1.687 \times 10^{-3}$	$1.241 \times 10^{-7}$	0.0289	$1.810 \times 10^{-4}$
25	13534	139.4	8.51533	$4.514 \times 10^{-6}$	$1.534 \times 10^{-3}$	$1.133 \times 10^{-7}$	0.0251	$1.810 \times 10^{-4}$
50	13473	138.6	8.83632	$4.734 \times 10^{-6}$	$1.423 \times 10^{-3}$	$1.056 \times 10^{-7}$	0.0223	$1.810 \times 10^{-4}$
75	13412	137.8	9.15632	$4.956 \times 10^{-6}$	$1.316 \times 10^{-3}$	$9.819 \times 10^{-8}$	0.0198	$1.810 \times 10^{-4}$
100	13351	137.1	9.46706	$5.170 \times 10^{-6}$	$1.245 \times 10^{-3}$	$9.326 \times 10^{-8}$	0.0180	$1.810 \times 10^{-4}$
150	13231	136.1	10.07780	$5.595 \times 10^{-6}$	$1.126 \times 10^{-3}$	$8.514 \times 10^{-8}$	0.0152	$1.810 \times 10^{-4}$
200	13112	135.5	10.65465	$5.996 \times 10^{-6}$	$1.043 \times 10^{-3}$	$7.959 \times 10^{-8}$	0.0133	$1.815 \times 10^{-4}$
250	12993	135.3	11.18150	$6.363 \times 10^{-6}$	$9.820 \times 10^{-4}$	$7.558 \times 10^{-8}$	0.0119	$1.829 \times 10^{-4}$
300	12873	135.3	11.68150	$6.705 \times 10^{-6}$	$9.336 \times 10^{-4}$	$7.252 \times 10^{-8}$	0.0108	$1.854 \times 10^{-4}$
<i>Bismuth (Bi) Melting Point: <math>271^\circ\text{C}</math></i>								
350	9969	146.0	16.28	$1.118 \times 10^{-5}$	$1.540 \times 10^{-3}$	$1.545 \times 10^{-7}$	0.01381	
400	9908	148.2	16.10	$1.096 \times 10^{-5}$	$1.422 \times 10^{-3}$	$1.436 \times 10^{-7}$	0.01310	
500	9785	152.8	15.74	$1.052 \times 10^{-5}$	$1.188 \times 10^{-3}$	$1.215 \times 10^{-7}$	0.01154	
600	9663	157.3	15.60	$1.026 \times 10^{-5}$	$1.013 \times 10^{-3}$	$1.048 \times 10^{-7}$	0.01022	
700	9540	161.8	15.60	$1.010 \times 10^{-5}$	$8.736 \times 10^{-4}$	$9.157 \times 10^{-8}$	0.00906	
<i>Lead (Pb) Melting Point: <math>327^\circ\text{C}</math></i>								
400	10506	158	15.97	$9.623 \times 10^{-6}$	$2.277 \times 10^{-3}$	$2.167 \times 10^{-7}$	0.02252	
450	10449	156	15.74	$9.649 \times 10^{-6}$	$2.065 \times 10^{-3}$	$1.976 \times 10^{-7}$	0.02048	
500	10390	155	15.54	$9.651 \times 10^{-6}$	$1.884 \times 10^{-3}$	$1.814 \times 10^{-7}$	0.01879	
550	10329	155	15.39	$9.610 \times 10^{-6}$	$1.758 \times 10^{-3}$	$1.702 \times 10^{-7}$	0.01771	
600	10267	155	15.23	$9.568 \times 10^{-6}$	$1.632 \times 10^{-3}$	$1.589 \times 10^{-7}$	0.01661	
650	10206	155	15.07	$9.526 \times 10^{-6}$	$1.505 \times 10^{-3}$	$1.475 \times 10^{-7}$	0.01549	
700	10145	155	14.91	$9.483 \times 10^{-6}$	$1.379 \times 10^{-3}$	$1.360 \times 10^{-7}$	0.01434	
<i>Sodium (Na) Melting Point: <math>98^\circ\text{C}</math></i>								
100	927.3	1378	85.84	$6.718 \times 10^{-5}$	$6.892 \times 10^{-4}$	$7.432 \times 10^{-7}$	0.01106	
200	902.5	1349	80.84	$6.639 \times 10^{-5}$	$5.385 \times 10^{-4}$	$5.967 \times 10^{-7}$	0.008987	
300	877.8	1320	75.84	$6.544 \times 10^{-5}$	$3.878 \times 10^{-4}$	$4.418 \times 10^{-7}$	0.006751	
400	853.0	1296	71.20	$6.437 \times 10^{-5}$	$2.720 \times 10^{-4}$	$3.188 \times 10^{-7}$	0.004953	
500	828.5	1284	67.41	$6.335 \times 10^{-5}$	$2.411 \times 10^{-4}$	$2.909 \times 10^{-7}$	0.004593	
600	804.0	1272	63.63	$6.220 \times 10^{-5}$	$2.101 \times 10^{-4}$	$2.614 \times 10^{-7}$	0.004202	
<i>Potassium (K) Melting Point: <math>64^\circ\text{C}</math></i>								
200	795.2	790.8	43.99	$6.995 \times 10^{-5}$	$3.350 \times 10^{-4}$	$4.213 \times 10^{-7}$	0.006023	
300	771.6	772.8	42.01	$7.045 \times 10^{-5}$	$2.667 \times 10^{-4}$	$3.456 \times 10^{-7}$	0.004906	
400	748.0	754.8	40.03	$7.090 \times 10^{-5}$	$1.984 \times 10^{-4}$	$2.652 \times 10^{-7}$	0.00374	
500	723.9	750.0	37.81	$6.964 \times 10^{-5}$	$1.668 \times 10^{-4}$	$2.304 \times 10^{-7}$	0.003309	
600	699.6	750.0	35.50	$6.765 \times 10^{-5}$	$1.487 \times 10^{-4}$	$2.126 \times 10^{-7}$	0.003143	
<i>Sodium-Potassium (%22Na-%78K) Melting Point: <math>-11^\circ\text{C}</math></i>								
100	847.3	944.4	25.64	$3.205 \times 10^{-5}$	$5.707 \times 10^{-4}$	$6.736 \times 10^{-7}$	0.02102	
200	823.2	922.5	26.27	$3.459 \times 10^{-5}$	$4.587 \times 10^{-4}$	$5.572 \times 10^{-7}$	0.01611	
300	799.1	900.6	26.89	$3.736 \times 10^{-5}$	$3.467 \times 10^{-4}$	$4.339 \times 10^{-7}$	0.01161	
400	775.0	879.0	27.50	$4.037 \times 10^{-5}$	$2.357 \times 10^{-4}$	$3.041 \times 10^{-7}$	0.00753	
500	751.5	880.1	27.89	$4.217 \times 10^{-5}$	$2.108 \times 10^{-4}$	$2.805 \times 10^{-7}$	0.00665	
600	728.0	881.2	28.28	$4.408 \times 10^{-5}$	$1.859 \times 10^{-4}$	$2.553 \times 10^{-7}$	0.00579	

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-15

Properties of air at 1 atm pressure

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
-150	2.866	983	0.01171	$4.158 \times 10^{-6}$	$8.636 \times 10^{-6}$	$3.013 \times 10^{-6}$	0.7246
-100	2.038	966	0.01582	$8.036 \times 10^{-6}$	$1.189 \times 10^{-5}$	$5.837 \times 10^{-6}$	0.7263
-50	1.582	999	0.01979	$1.252 \times 10^{-5}$	$1.474 \times 10^{-5}$	$9.319 \times 10^{-6}$	0.7440
-40	1.514	1002	0.02057	$1.356 \times 10^{-5}$	$1.527 \times 10^{-5}$	$1.008 \times 10^{-5}$	0.7436
-30	1.451	1004	0.02134	$1.465 \times 10^{-5}$	$1.579 \times 10^{-5}$	$1.087 \times 10^{-5}$	0.7425
-20	1.394	1005	0.02211	$1.578 \times 10^{-5}$	$1.630 \times 10^{-5}$	$1.169 \times 10^{-5}$	0.7408
-10	1.341	1006	0.02288	$1.696 \times 10^{-5}$	$1.680 \times 10^{-5}$	$1.252 \times 10^{-5}$	0.7387
0	1.292	1006	0.02364	$1.818 \times 10^{-5}$	$1.729 \times 10^{-5}$	$1.338 \times 10^{-5}$	0.7362
5	1.269	1006	0.02401	$1.880 \times 10^{-5}$	$1.754 \times 10^{-5}$	$1.382 \times 10^{-5}$	0.7350
10	1.246	1006	0.02439	$1.944 \times 10^{-5}$	$1.778 \times 10^{-5}$	$1.426 \times 10^{-5}$	0.7336
15	1.225	1007	0.02476	$2.009 \times 10^{-5}$	$1.802 \times 10^{-5}$	$1.470 \times 10^{-5}$	0.7323
20	1.204	1007	0.02514	$2.074 \times 10^{-5}$	$1.825 \times 10^{-5}$	$1.516 \times 10^{-5}$	0.7309
25	1.184	1007	0.02551	$2.141 \times 10^{-5}$	$1.849 \times 10^{-5}$	$1.562 \times 10^{-5}$	0.7296
30	1.164	1007	0.02588	$2.208 \times 10^{-5}$	$1.872 \times 10^{-5}$	$1.608 \times 10^{-5}$	0.7282
35	1.145	1007	0.02625	$2.277 \times 10^{-5}$	$1.895 \times 10^{-5}$	$1.655 \times 10^{-5}$	0.7268
40	1.127	1007	0.02662	$2.346 \times 10^{-5}$	$1.918 \times 10^{-5}$	$1.702 \times 10^{-5}$	0.7255
45	1.109	1007	0.02699	$2.416 \times 10^{-5}$	$1.941 \times 10^{-5}$	$1.750 \times 10^{-5}$	0.7241
50	1.092	1007	0.02735	$2.487 \times 10^{-5}$	$1.963 \times 10^{-5}$	$1.798 \times 10^{-5}$	0.7228
60	1.059	1007	0.02808	$2.632 \times 10^{-5}$	$2.008 \times 10^{-5}$	$1.896 \times 10^{-5}$	0.7202
70	1.028	1007	0.02881	$2.780 \times 10^{-5}$	$2.052 \times 10^{-5}$	$1.995 \times 10^{-5}$	0.7177
80	0.9994	1008	0.02953	$2.931 \times 10^{-5}$	$2.096 \times 10^{-5}$	$2.097 \times 10^{-5}$	0.7154
90	0.9718	1008	0.03024	$3.086 \times 10^{-5}$	$2.139 \times 10^{-5}$	$2.201 \times 10^{-5}$	0.7132
100	0.9458	1009	0.03095	$3.243 \times 10^{-5}$	$2.181 \times 10^{-5}$	$2.306 \times 10^{-5}$	0.7111
120	0.8977	1011	0.03235	$3.565 \times 10^{-5}$	$2.264 \times 10^{-5}$	$2.522 \times 10^{-5}$	0.7073
140	0.8542	1013	0.03374	$3.898 \times 10^{-5}$	$2.345 \times 10^{-5}$	$2.745 \times 10^{-5}$	0.7041
160	0.8148	1016	0.03511	$4.241 \times 10^{-5}$	$2.420 \times 10^{-5}$	$2.975 \times 10^{-5}$	0.7014
180	0.7788	1019	0.03646	$4.593 \times 10^{-5}$	$2.504 \times 10^{-5}$	$3.212 \times 10^{-5}$	0.6992
200	0.7459	1023	0.03779	$4.954 \times 10^{-5}$	$2.577 \times 10^{-5}$	$3.455 \times 10^{-5}$	0.6974
250	0.6746	1033	0.04104	$5.890 \times 10^{-5}$	$2.760 \times 10^{-5}$	$4.091 \times 10^{-5}$	0.6946
300	0.6158	1044	0.04418	$6.871 \times 10^{-5}$	$2.934 \times 10^{-5}$	$4.765 \times 10^{-5}$	0.6935
350	0.5664	1056	0.04721	$7.892 \times 10^{-5}$	$3.101 \times 10^{-5}$	$5.475 \times 10^{-5}$	0.6937
400	0.5243	1069	0.05015	$8.951 \times 10^{-5}$	$3.261 \times 10^{-5}$	$6.219 \times 10^{-5}$	0.6948
450	0.4880	1081	0.05298	$1.004 \times 10^{-4}$	$3.415 \times 10^{-5}$	$6.997 \times 10^{-5}$	0.6965
500	0.4565	1093	0.05572	$1.117 \times 10^{-4}$	$3.563 \times 10^{-5}$	$7.806 \times 10^{-5}$	0.6986
600	0.4042	1115	0.06093	$1.352 \times 10^{-4}$	$3.846 \times 10^{-5}$	$9.515 \times 10^{-5}$	0.7037
700	0.3627	1135	0.06581	$1.598 \times 10^{-4}$	$4.111 \times 10^{-5}$	$1.133 \times 10^{-4}$	0.7092
800	0.3289	1153	0.07037	$1.855 \times 10^{-4}$	$4.362 \times 10^{-5}$	$1.326 \times 10^{-4}$	0.7149
900	0.3008	1169	0.07465	$2.122 \times 10^{-4}$	$4.600 \times 10^{-5}$	$1.529 \times 10^{-4}$	0.7206
1000	0.2772	1184	0.07868	$2.398 \times 10^{-4}$	$4.826 \times 10^{-5}$	$1.741 \times 10^{-4}$	0.7260
1500	0.1990	1234	0.09599	$3.908 \times 10^{-4}$	$5.817 \times 10^{-5}$	$2.922 \times 10^{-4}$	0.7478
2000	0.1553	1264	0.11113	$5.664 \times 10^{-4}$	$6.630 \times 10^{-5}$	$4.270 \times 10^{-4}$	0.7539

Note: For ideal gases, the properties  $c_p$ ,  $k$ ,  $\mu$ , and Pr are independent of pressure. The properties  $\rho$ ,  $\nu$ , and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $\rho$  at the given temperature by  $P$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Keenan, Chao, Keyes, Gas Tables, Wiley, 1984; and Thermophysical Properties of Matter. Vol. 3: Thermal Conductivity, Y. S. Touloukian, P. E. Liley, S. C. Saxena, Vol. 11: Viscosity, Y. S. Touloukian, S. C. Saxena, and P. Hestermans, IFI/Plenum, NY, 1970, ISBN 0-306067020-8.

TABLE A-16

Properties of gases at 1 atm pressure

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
<i>Carbon Dioxide, CO<sub>2</sub></i>							
-50	2.4035	746	0.01051	$5.860 \times 10^{-6}$	$1.129 \times 10^{-5}$	$4.699 \times 10^{-6}$	0.8019
0	1.9635	811	0.01456	$9.141 \times 10^{-6}$	$1.375 \times 10^{-5}$	$7.003 \times 10^{-6}$	0.7661
50	1.6597	866.6	0.01858	$1.291 \times 10^{-5}$	$1.612 \times 10^{-5}$	$9.714 \times 10^{-6}$	0.7520
100	1.4373	914.8	0.02257	$1.716 \times 10^{-5}$	$1.841 \times 10^{-5}$	$1.281 \times 10^{-5}$	0.7464
150	1.2675	957.4	0.02652	$2.186 \times 10^{-5}$	$2.063 \times 10^{-5}$	$1.627 \times 10^{-5}$	0.7445
200	1.1336	995.2	0.03044	$2.698 \times 10^{-5}$	$2.276 \times 10^{-5}$	$2.008 \times 10^{-5}$	0.7442
300	0.9358	1060	0.03814	$3.847 \times 10^{-5}$	$2.682 \times 10^{-5}$	$2.866 \times 10^{-5}$	0.7450
400	0.7968	1112	0.04565	$5.151 \times 10^{-5}$	$3.061 \times 10^{-5}$	$3.842 \times 10^{-5}$	0.7458
500	0.6937	1156	0.05293	$6.600 \times 10^{-5}$	$3.416 \times 10^{-5}$	$4.924 \times 10^{-5}$	0.7460
1000	0.4213	1292	0.08491	$1.560 \times 10^{-4}$	$4.898 \times 10^{-5}$	$1.162 \times 10^{-4}$	0.7455
1500	0.3025	1356	0.10688	$2.606 \times 10^{-4}$	$6.106 \times 10^{-5}$	$2.019 \times 10^{-4}$	0.7745
2000	0.2359	1387	0.11522	$3.521 \times 10^{-4}$	$7.322 \times 10^{-5}$	$3.103 \times 10^{-4}$	0.8815
<i>Carbon Monoxide, CO</i>							
-50	1.5297	1081	0.01901	$1.149 \times 10^{-5}$	$1.378 \times 10^{-5}$	$9.012 \times 10^{-6}$	0.7840
0	1.2497	1048	0.02278	$1.739 \times 10^{-5}$	$1.629 \times 10^{-5}$	$1.303 \times 10^{-5}$	0.7499
50	1.0563	1039	0.02641	$2.407 \times 10^{-5}$	$1.863 \times 10^{-5}$	$1.764 \times 10^{-5}$	0.7328
100	0.9148	1041	0.02992	$3.142 \times 10^{-5}$	$2.080 \times 10^{-5}$	$2.274 \times 10^{-5}$	0.7239
150	0.8067	1049	0.03330	$3.936 \times 10^{-5}$	$2.283 \times 10^{-5}$	$2.830 \times 10^{-5}$	0.7191
200	0.7214	1060	0.03656	$4.782 \times 10^{-5}$	$2.472 \times 10^{-5}$	$3.426 \times 10^{-5}$	0.7164
300	0.5956	1085	0.04277	$6.619 \times 10^{-5}$	$2.812 \times 10^{-5}$	$4.722 \times 10^{-5}$	0.7134
400	0.5071	1111	0.04860	$8.628 \times 10^{-5}$	$3.111 \times 10^{-5}$	$6.136 \times 10^{-5}$	0.7111
500	0.4415	1135	0.05412	$1.079 \times 10^{-4}$	$3.379 \times 10^{-5}$	$7.653 \times 10^{-5}$	0.7087
1000	0.2681	1226	0.07894	$2.401 \times 10^{-4}$	$4.557 \times 10^{-5}$	$1.700 \times 10^{-4}$	0.7080
1500	0.1925	1279	0.10458	$4.246 \times 10^{-4}$	$6.321 \times 10^{-5}$	$3.284 \times 10^{-4}$	0.7733
2000	0.1502	1309	0.13833	$7.034 \times 10^{-4}$	$9.826 \times 10^{-5}$	$6.543 \times 10^{-4}$	0.9302
<i>Methane, CH<sub>4</sub></i>							
-50	0.8761	2243	0.02367	$1.204 \times 10^{-5}$	$8.564 \times 10^{-6}$	$9.774 \times 10^{-6}$	0.8116
0	0.7158	2217	0.03042	$1.917 \times 10^{-5}$	$1.028 \times 10^{-5}$	$1.436 \times 10^{-5}$	0.7494
50	0.6050	2302	0.03766	$2.704 \times 10^{-5}$	$1.191 \times 10^{-5}$	$1.969 \times 10^{-5}$	0.7282
100	0.5240	2443	0.04534	$3.543 \times 10^{-5}$	$1.345 \times 10^{-5}$	$2.567 \times 10^{-5}$	0.7247
150	0.4620	2611	0.05344	$4.431 \times 10^{-5}$	$1.491 \times 10^{-5}$	$3.227 \times 10^{-5}$	0.7284
200	0.4132	2791	0.06194	$5.370 \times 10^{-5}$	$1.630 \times 10^{-5}$	$3.944 \times 10^{-5}$	0.7344
300	0.3411	3158	0.07996	$7.422 \times 10^{-5}$	$1.886 \times 10^{-5}$	$5.529 \times 10^{-5}$	0.7450
400	0.2904	3510	0.09918	$9.727 \times 10^{-5}$	$2.119 \times 10^{-5}$	$7.297 \times 10^{-5}$	0.7501
500	0.2529	3836	0.11933	$1.230 \times 10^{-4}$	$2.334 \times 10^{-5}$	$9.228 \times 10^{-5}$	0.7502
1000	0.1536	5042	0.22562	$2.914 \times 10^{-4}$	$3.281 \times 10^{-5}$	$2.136 \times 10^{-4}$	0.7331
1500	0.1103	5701	0.31857	$5.068 \times 10^{-4}$	$4.434 \times 10^{-5}$	$4.022 \times 10^{-4}$	0.7936
2000	0.0860	6001	0.36750	$7.120 \times 10^{-4}$	$6.360 \times 10^{-5}$	$7.395 \times 10^{-4}$	1.0386
<i>Hydrogen, H<sub>2</sub></i>							
-50	0.11010	12635	0.1404	$1.009 \times 10^{-4}$	$7.293 \times 10^{-6}$	$6.624 \times 10^{-5}$	0.6562
0	0.08995	13920	0.1652	$1.319 \times 10^{-4}$	$8.391 \times 10^{-6}$	$9.329 \times 10^{-5}$	0.7071
50	0.07603	14349	0.1881	$1.724 \times 10^{-4}$	$9.427 \times 10^{-6}$	$1.240 \times 10^{-4}$	0.7191
100	0.06584	14473	0.2095	$2.199 \times 10^{-4}$	$1.041 \times 10^{-5}$	$1.582 \times 10^{-4}$	0.7196
150	0.05806	14492	0.2296	$2.729 \times 10^{-4}$	$1.136 \times 10^{-5}$	$1.957 \times 10^{-4}$	0.7174
200	0.05193	14482	0.2486	$3.306 \times 10^{-4}$	$1.228 \times 10^{-5}$	$2.365 \times 10^{-4}$	0.7155

TABLE A-16

Properties of gases at 1 atm pressure (Concluded)

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
300	0.04287	14481	0.2843	$4.580 \times 10^{-4}$	$1.403 \times 10^{-5}$	$3.274 \times 10^{-4}$	0.7149
400	0.03650	14540	0.3180	$5.992 \times 10^{-4}$	$1.570 \times 10^{-5}$	$4.302 \times 10^{-4}$	0.7179
500	0.03178	14653	0.3509	$7.535 \times 10^{-4}$	$1.730 \times 10^{-5}$	$5.443 \times 10^{-4}$	0.7224
1000	0.01930	15577	0.5206	$1.732 \times 10^{-3}$	$2.455 \times 10^{-5}$	$1.272 \times 10^{-3}$	0.7345
1500	0.01386	16553	0.6581	$2.869 \times 10^{-3}$	$3.099 \times 10^{-5}$	$2.237 \times 10^{-3}$	0.7795
2000	0.01081	17400	0.5480	$2.914 \times 10^{-3}$	$3.690 \times 10^{-5}$	$3.414 \times 10^{-3}$	1.1717
<i>Nitrogen, N<sub>2</sub></i>							
-50	1.5299	957.3	0.02001	$1.366 \times 10^{-5}$	$1.390 \times 10^{-5}$	$9.091 \times 10^{-6}$	0.6655
0	1.2498	1035	0.02384	$1.843 \times 10^{-5}$	$1.640 \times 10^{-5}$	$1.312 \times 10^{-5}$	0.7121
50	1.0564	1042	0.02746	$2.494 \times 10^{-5}$	$1.874 \times 10^{-5}$	$1.774 \times 10^{-5}$	0.7114
100	0.9149	1041	0.03090	$3.244 \times 10^{-5}$	$2.094 \times 10^{-5}$	$2.289 \times 10^{-5}$	0.7056
150	0.8068	1043	0.03416	$4.058 \times 10^{-5}$	$2.300 \times 10^{-5}$	$2.851 \times 10^{-5}$	0.7025
200	0.7215	1050	0.03727	$4.921 \times 10^{-5}$	$2.494 \times 10^{-5}$	$3.457 \times 10^{-5}$	0.7025
300	0.5956	1070	0.04309	$6.758 \times 10^{-5}$	$2.849 \times 10^{-5}$	$4.783 \times 10^{-5}$	0.7078
400	0.5072	1095	0.04848	$8.727 \times 10^{-5}$	$3.166 \times 10^{-5}$	$6.242 \times 10^{-5}$	0.7153
500	0.4416	1120	0.05358	$1.083 \times 10^{-4}$	$3.451 \times 10^{-5}$	$7.816 \times 10^{-5}$	0.7215
1000	0.2681	1213	0.07938	$2.440 \times 10^{-4}$	$4.594 \times 10^{-5}$	$1.713 \times 10^{-4}$	0.7022
1500	0.1925	1266	0.11793	$4.839 \times 10^{-4}$	$5.562 \times 10^{-5}$	$2.889 \times 10^{-4}$	0.5969
2000	0.1502	1297	0.18590	$9.543 \times 10^{-4}$	$6.426 \times 10^{-5}$	$4.278 \times 10^{-4}$	0.4483
<i>Oxygen, O<sub>2</sub></i>							
-50	1.7475	984.4	0.02067	$1.201 \times 10^{-5}$	$1.616 \times 10^{-5}$	$9.246 \times 10^{-6}$	0.7694
0	1.4277	928.7	0.02472	$1.865 \times 10^{-5}$	$1.916 \times 10^{-5}$	$1.342 \times 10^{-5}$	0.7198
50	1.2068	921.7	0.02867	$2.577 \times 10^{-5}$	$2.194 \times 10^{-5}$	$1.818 \times 10^{-5}$	0.7053
100	1.0451	931.8	0.03254	$3.342 \times 10^{-5}$	$2.451 \times 10^{-5}$	$2.346 \times 10^{-5}$	0.7019
150	0.9216	947.6	0.03637	$4.164 \times 10^{-5}$	$2.694 \times 10^{-5}$	$2.923 \times 10^{-5}$	0.7019
200	0.8242	964.7	0.04014	$5.048 \times 10^{-5}$	$2.923 \times 10^{-5}$	$3.546 \times 10^{-5}$	0.7025
300	0.6804	997.1	0.04751	$7.003 \times 10^{-5}$	$3.350 \times 10^{-5}$	$4.923 \times 10^{-5}$	0.7030
400	0.5793	1025	0.05463	$9.204 \times 10^{-5}$	$3.744 \times 10^{-5}$	$6.463 \times 10^{-5}$	0.7023
500	0.5044	1048	0.06148	$1.163 \times 10^{-4}$	$4.114 \times 10^{-5}$	$8.156 \times 10^{-5}$	0.7010
1000	0.3063	1121	0.09198	$2.678 \times 10^{-4}$	$5.732 \times 10^{-5}$	$1.871 \times 10^{-4}$	0.6986
1500	0.2199	1165	0.11901	$4.643 \times 10^{-4}$	$7.133 \times 10^{-5}$	$3.243 \times 10^{-4}$	0.6985
2000	0.1716	1201	0.14705	$7.139 \times 10^{-4}$	$8.417 \times 10^{-5}$	$4.907 \times 10^{-4}$	0.6873
<i>Water Vapor, H<sub>2</sub>O</i>							
-50	0.9839	1892	0.01353	$7.271 \times 10^{-6}$	$7.187 \times 10^{-6}$	$7.305 \times 10^{-6}$	1.0047
0	0.8038	1874	0.01673	$1.110 \times 10^{-5}$	$8.956 \times 10^{-6}$	$1.114 \times 10^{-5}$	1.0033
50	0.6794	1874	0.02032	$1.596 \times 10^{-5}$	$1.078 \times 10^{-5}$	$1.587 \times 10^{-5}$	0.9944
100	0.5884	1887	0.02429	$2.187 \times 10^{-5}$	$1.265 \times 10^{-5}$	$2.150 \times 10^{-5}$	0.9830
150	0.5189	1908	0.02861	$2.890 \times 10^{-5}$	$1.456 \times 10^{-5}$	$2.806 \times 10^{-5}$	0.9712
200	0.4640	1935	0.03326	$3.705 \times 10^{-5}$	$1.650 \times 10^{-5}$	$3.556 \times 10^{-5}$	0.9599
300	0.3831	1997	0.04345	$5.680 \times 10^{-5}$	$2.045 \times 10^{-5}$	$5.340 \times 10^{-5}$	0.9401
400	0.3262	2066	0.05467	$8.114 \times 10^{-5}$	$2.446 \times 10^{-5}$	$7.498 \times 10^{-5}$	0.9240
500	0.2840	2137	0.06677	$1.100 \times 10^{-4}$	$2.847 \times 10^{-5}$	$1.002 \times 10^{-4}$	0.9108
1000	0.1725	2471	0.13623	$3.196 \times 10^{-4}$	$4.762 \times 10^{-5}$	$2.761 \times 10^{-4}$	0.8639
1500	0.1238	2736	0.21301	$6.288 \times 10^{-4}$	$6.411 \times 10^{-5}$	$5.177 \times 10^{-4}$	0.8233
2000	0.0966	2928	0.29183	$1.032 \times 10^{-3}$	$7.808 \times 10^{-5}$	$8.084 \times 10^{-4}$	0.7833

Note: For ideal gases, the properties  $c_p$ ,  $k$ ,  $\mu$ , and Pr are independent of pressure. The properties  $\rho$ ,  $\nu$ , and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $\rho$  at the given temperature by  $P$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-17

Properties of the atmosphere at high altitude

Altitude, $z$ , m	Temperature, $T$ , °C	Pressure, $P$ , kPa	Gravity $g$ , m/s <sup>2</sup>	Speed of Sound, $c$ , m/s	Density, $\rho$ , kg/m <sup>3</sup>	Viscosity $\mu$ , kg/m·s	Thermal Conductivity, $k$ , W/m·K
0	15.00	101.33	9.807	340.3	1.225	$1.789 \times 10^{-5}$	0.0253
200	13.70	98.95	9.806	339.5	1.202	$1.783 \times 10^{-5}$	0.0252
400	12.40	96.61	9.805	338.8	1.179	$1.777 \times 10^{-5}$	0.0252
600	11.10	94.32	9.805	338.0	1.156	$1.771 \times 10^{-5}$	0.0251
800	9.80	92.08	9.804	337.2	1.134	$1.764 \times 10^{-5}$	0.0250
1000	8.50	89.88	9.804	336.4	1.112	$1.758 \times 10^{-5}$	0.0249
1200	7.20	87.72	9.803	335.7	1.090	$1.752 \times 10^{-5}$	0.0248
1400	5.90	85.60	9.802	334.9	1.069	$1.745 \times 10^{-5}$	0.0247
1600	4.60	83.53	9.802	334.1	1.048	$1.739 \times 10^{-5}$	0.0245
1800	3.30	81.49	9.801	333.3	1.027	$1.732 \times 10^{-5}$	0.0244
2000	2.00	79.50	9.800	332.5	1.007	$1.726 \times 10^{-5}$	0.0243
2200	0.70	77.55	9.800	331.7	0.987	$1.720 \times 10^{-5}$	0.0242
2400	-0.59	75.63	9.799	331.0	0.967	$1.713 \times 10^{-5}$	0.0241
2600	-1.89	73.76	9.799	330.2	0.947	$1.707 \times 10^{-5}$	0.0240
2800	-3.19	71.92	9.798	329.4	0.928	$1.700 \times 10^{-5}$	0.0239
3000	-4.49	70.12	9.797	328.6	0.909	$1.694 \times 10^{-5}$	0.0238
3200	-5.79	68.36	9.797	327.8	0.891	$1.687 \times 10^{-5}$	0.0237
3400	-7.09	66.63	9.796	327.0	0.872	$1.681 \times 10^{-5}$	0.0236
3600	-8.39	64.94	9.796	326.2	0.854	$1.674 \times 10^{-5}$	0.0235
3800	-9.69	63.28	9.795	325.4	0.837	$1.668 \times 10^{-5}$	0.0234
4000	-10.98	61.66	9.794	324.6	0.819	$1.661 \times 10^{-5}$	0.0233
4200	-12.3	60.07	9.794	323.8	0.802	$1.655 \times 10^{-5}$	0.0232
4400	-13.6	58.52	9.793	323.0	0.785	$1.648 \times 10^{-5}$	0.0231
4600	-14.9	57.00	9.793	322.2	0.769	$1.642 \times 10^{-5}$	0.0230
4800	-16.2	55.51	9.792	321.4	0.752	$1.635 \times 10^{-5}$	0.0229
5000	-17.5	54.05	9.791	320.5	0.736	$1.628 \times 10^{-5}$	0.0228
5200	-18.8	52.62	9.791	319.7	0.721	$1.622 \times 10^{-5}$	0.0227
5400	-20.1	51.23	9.790	318.9	0.705	$1.615 \times 10^{-5}$	0.0226
5600	-21.4	49.86	9.789	318.1	0.690	$1.608 \times 10^{-5}$	0.0224
5800	-22.7	48.52	9.785	317.3	0.675	$1.602 \times 10^{-5}$	0.0223
6000	-24.0	47.22	9.788	316.5	0.660	$1.595 \times 10^{-5}$	0.0222
6200	-25.3	45.94	9.788	315.6	0.646	$1.588 \times 10^{-5}$	0.0221
6400	-26.6	44.69	9.787	314.8	0.631	$1.582 \times 10^{-5}$	0.0220
6600	-27.9	43.47	9.786	314.0	0.617	$1.575 \times 10^{-5}$	0.0219
6800	-29.2	42.27	9.785	313.1	0.604	$1.568 \times 10^{-5}$	0.0218
7000	-30.5	41.11	9.785	312.3	0.590	$1.561 \times 10^{-5}$	0.0217
8000	-36.9	35.65	9.782	308.1	0.526	$1.527 \times 10^{-5}$	0.0212
9000	-43.4	30.80	9.779	303.8	0.467	$1.493 \times 10^{-5}$	0.0206
10,000	-49.9	26.50	9.776	299.5	0.414	$1.458 \times 10^{-5}$	0.0201
12,000	-56.5	19.40	9.770	295.1	0.312	$1.422 \times 10^{-5}$	0.0195
14,000	-56.5	14.17	9.764	295.1	0.228	$1.422 \times 10^{-5}$	0.0195
16,000	-56.5	10.53	9.758	295.1	0.166	$1.422 \times 10^{-5}$	0.0195
18,000	-56.5	7.57	9.751	295.1	0.122	$1.422 \times 10^{-5}$	0.0195

Source: U.S. Standard Atmosphere Supplements, U.S. Government Printing Office, 1966. Based on year-round mean conditions at 45° latitude and varies with the time of the year and the weather patterns. The conditions at sea level ( $z = 0$ ) are taken to be  $P = 101.325$  kPa,  $T = 15^\circ\text{C}$ ,  $\rho = 1.2250$  kg/m<sup>3</sup>,  $g = 9.80665$  m/s<sup>2</sup>.

TABLE A-18

Emissivities of surfaces

(a) Metals

Material	Temperature, K	Emissivity, $\varepsilon$	Material	Temperature, K	Emissivity, $\varepsilon$
Aluminum			Magnesium, polished	300–500	0.07–0.13
Polished	300–900	0.04–0.06	Mercury	300–400	0.09–0.12
Commercial sheet	400	0.09	Molybdenum		
Heavily oxidized	400–800	0.20–0.33	Polished	300–2000	0.05–0.21
Anodized	300	0.8	Oxidized	600–800	0.80–0.82
Bismuth, bright	350	0.34	Nickel		
Brass			Polished	500–1200	0.07–0.17
Highly polished	500–650	0.03–0.04	Oxidized	450–1000	0.37–0.57
Polished	350	0.09	Platinum, polished	500–1500	0.06–0.18
Dull plate	300–600	0.22	Silver, polished	300–1000	0.02–0.07
Oxidized	450–800	0.6	Stainless steel		
Chromium, polished	300–1400	0.08–0.40	Polished	300–1000	0.17–0.30
Copper			Lightly oxidized	600–1000	0.30–0.40
Highly polished	300	0.02	Highly oxidized	600–1000	0.70–0.80
Polished	300–500	0.04–0.05	Steel		
Commercial sheet	300	0.15	Polished sheet	300–500	0.08–0.14
Oxidized	600–1000	0.5–0.8	Commercial sheet	500–1200	0.20–0.32
Black oxidized	300	0.78	Heavily oxidized	300	0.81
Gold			Tin, polished	300	0.05
Highly polished	300–1000	0.03–0.06	Tungsten		
Bright foil	300	0.07	Polished	300–2500	0.03–0.29
Iron			Filament	3500	0.39
Highly polished	300–500	0.05–0.07	Zinc		
Case iron	300	0.44	Polished	300–800	0.02–0.05
Wrought iron	300–500	0.28	Oxidized	300	0.25
Rusted	300	0.61			
Oxidized	500–900	0.64–0.78			
Lead					
Polished	300–500	0.06–0.08			
Unoxidized, rough	300	0.43			
Oxidized	300	0.63			



TABLE A-18

Emissivities of surfaces (*Concluded*)  
(*b*) Nonmetals

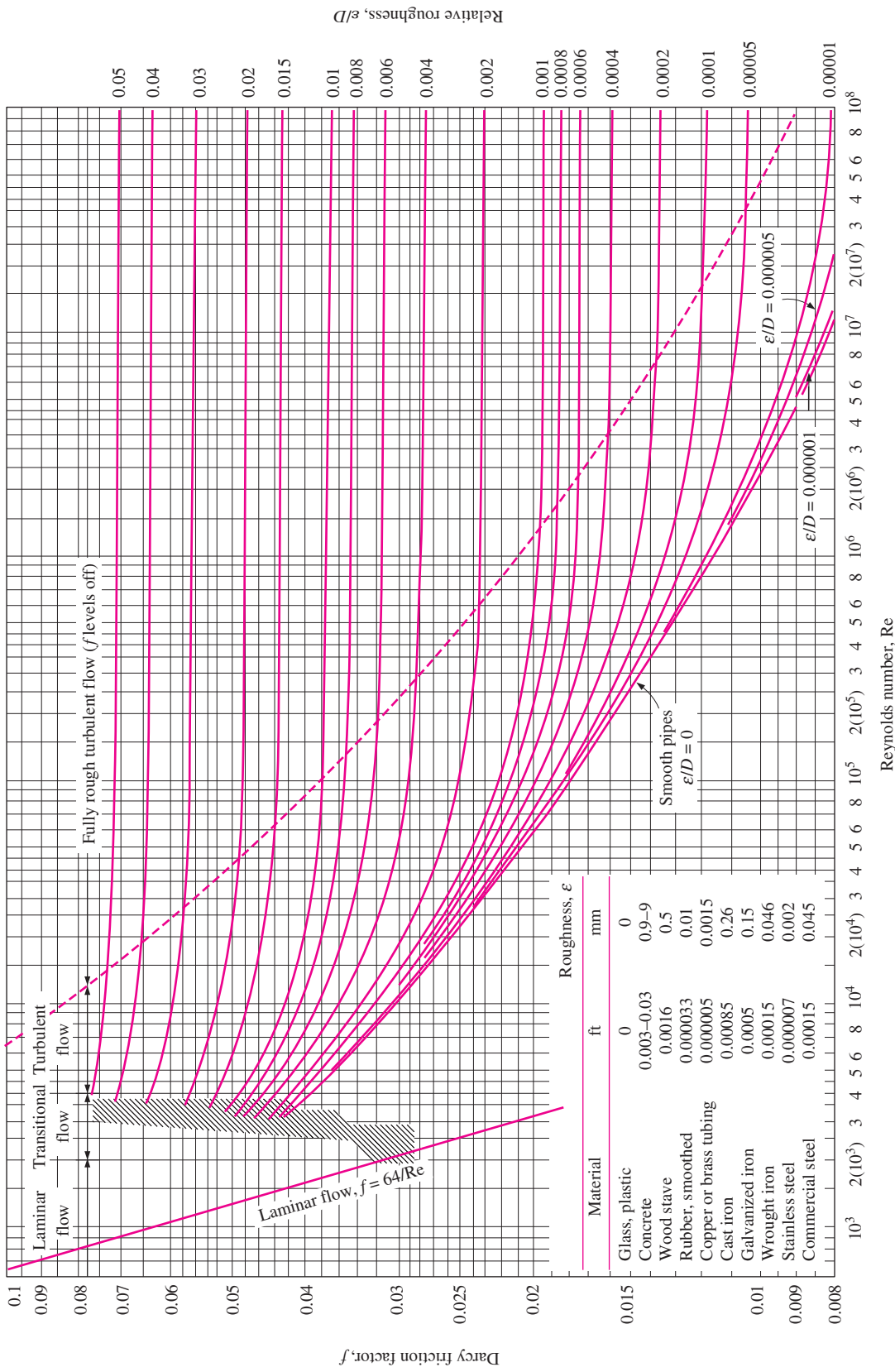
Material	Temperature, K	Emissivity, $\varepsilon$	Material	Temperature, K	Emissivity, $\varepsilon$
Alumina	800–1400	0.65–0.45	Paper, white	300	0.90
Aluminum oxide	600–1500	0.69–0.41	Plaster, white	300	0.93
Asbestos	300	0.96	Porcelain, glazed	300	0.92
Asphalt pavement	300	0.85–0.93	Quartz, rough, fused	300	0.93
Brick			Rubber		
Common	300	0.93–0.96	Hard	300	0.93
Fireclay	1200	0.75	Soft	300	0.86
Carbon filament	2000	0.53	Sand	300	0.90
Cloth	300	0.75–0.90	Silicon carbide	600–1500	0.87–0.85
Concrete	300	0.88–0.94	Skin, human	300	0.95
Glass			Snow	273	0.80–0.90
Window	300	0.90–0.95	Soil, earth	300	0.93–0.96
Pyrex	300–1200	0.82–0.62	Soot	300–500	0.95
Pyroceram	300–1500	0.85–0.57	Teflon	300–500	0.85–0.92
Ice	273	0.95–0.99	Water, deep	273–373	0.95–0.96
Magnesium oxide	400–800	0.69–0.55	Wood		
Masonry	300	0.80	Beech	300	0.94
Paints			Oak	300	0.90
Aluminum	300	0.40–0.50			
Black, lacquer, shiny	300	0.88			
Oils, all colors	300	0.92–0.96			
Red primer	300	0.93			
White acrylic	300	0.90			
White enamel	300	0.90			

TABLE A-19

Solar radiative properties of materials

Description/composition	Solar Absorptivity, $\alpha_s$	Emissivity, $\epsilon$ , at 300 K	Ratio, $\alpha_s/\epsilon$	Solar Transmissivity, $\tau_s$
Aluminum				
Polished	0.09	0.03	3.0	
Anodized	0.14	0.84	0.17	
Quartz-overcoated	0.11	0.37	0.30	
Foil	0.15	0.05	3.0	
Brick, red (Purdue)	0.63	0.93	0.68	
Concrete	0.60	0.88	0.68	
Galvanized sheet metal				
Clean, new	0.65	0.13	5.0	
Oxidized, weathered	0.80	0.28	2.9	
Glass, 3.2-mm thickness				
Float or tempered				0.79
Low iron oxide type				0.88
Marble, slightly off-white (nonreflective)	0.40	0.88	0.45	
Metal, plated				
Black sulfide	0.92	0.10	9.2	
Black cobalt oxide	0.93	0.30	3.1	
Black nickel oxide	0.92	0.08	11	
Black chrome	0.87	0.09	9.7	
Mylar, 0.13-mm thickness				0.87
Paints				
Black (Parsons)	0.98	0.98	1.0	
White, acrylic	0.26	0.90	0.29	
White, zinc oxide	0.16	0.93	0.17	
Paper, white	0.27	0.83	0.32	
Plexiglas, 3.2-mm thickness				0.90
Porcelain tiles, white (reflective glazed surface)	0.26	0.85	0.30	
Roofing tiles, bright red				
Dry surface	0.65	0.85	0.76	
Wet surface	0.88	0.91	0.96	
Sand, dry				
Off-white	0.52	0.82	0.63	
Dull red	0.73	0.86	0.82	
Snow				
Fine particles, fresh	0.13	0.82	0.16	
Ice granules	0.33	0.89	0.37	
Steel				
Mirror-finish	0.41	0.05	8.2	
Heavily rusted	0.89	0.92	0.96	
Stone (light pink)	0.65	0.87	0.74	
Tedlar, 0.10-mm thickness				0.92
Teflon, 0.13-mm thickness				0.92
Wood	0.59	0.90	0.66	

Source: V. C. Sharma and A. Sharma, "Solar Properties of Some Building Elements," *Energy* 14 (1989), pp. 805–810, and other sources.



**FIGURE A-20**

The Moody chart for the friction factor for fully developed flow in circular pipes for use in the head loss relation  $\Delta P_L = f \frac{L}{D} \frac{\rho V^2}{2}$ . Friction factors in the turbulent flow are evaluated from the Colebrook equation  $\frac{1}{\sqrt{f}} = -2 \log_{10} \left( \frac{\epsilon/D}{3.7} + \frac{2.51}{Re \sqrt{f}} \right)$ .